



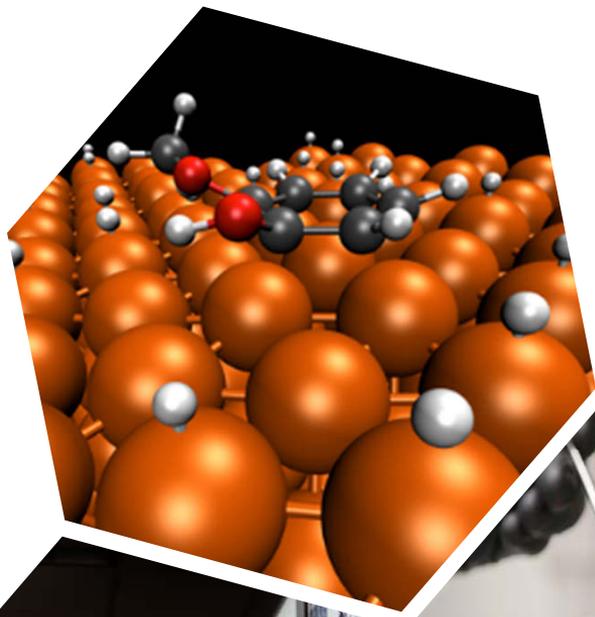
Recent Advancements in Catalytic Fast Pyrolysis for the Production of Fuels and Chemicals from Biomass

Joshua A. Schaidle, NREL

ePYRO 2021

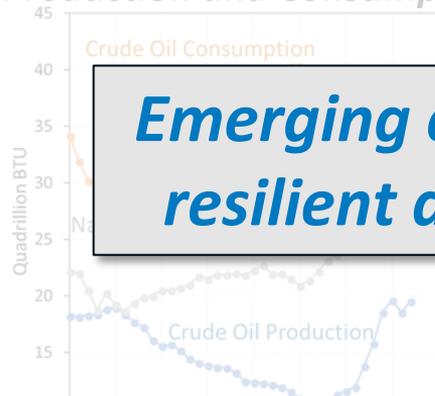
April 13th, 2021

NREL/PR-5100-79564



Trends in Carbon Management

Major Shifts in US Fossil Fuel Production and Consumption



Increased Electrification

Decreasing costs for renewable electricity

International Maritime Organization

Reduce sulfur in marine bunker fuel from 3.5% to 0.5% as of 2020

Emerging carbon conversion technologies need to be resilient and responsive to market and policy shifts



Need for Carbon-Negative

Challenge: How do we design carbon conversion technologies, including capex-intensive facilities, to succeed in tomorrow's dynamic economy?



Airlines for America



National Academy of Sciences

Opportunity: Designed Resilience

“It is not the strongest of the species that survives, nor the most intelligent, but the one most adaptable to change”
Leon C. Megginson

National Academy of Sciences Definition of Resilience: “The ability to prepare and plan for, absorb, recover from, and more successfully adapt to adverse events”

I. Linkov, et al., Changing the Resilience Paradigm, *Nature Climate Change* 4 (2014) 407.

Goal: Enable the design of *versatile catalytic carbon conversion technology platforms* capable of nimbly responding to external stimuli

Critical Needs:

- Feedstock flexibility
- Adaptive process design and control
- Low conversion costs
- Product tunability

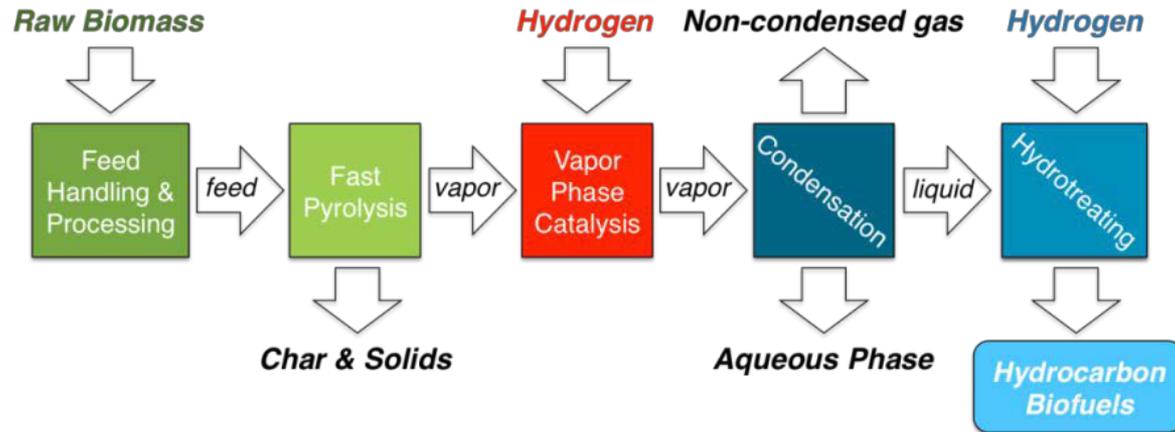
Porter's Five Forces

Exhibit
Forces governing competition in an industry



Catalytic Fast Pyrolysis (CFP) Technology Platform

Potential for whole biomass conversion to drop-in hydrocarbon fuels at high yields (>75 gal/ton)



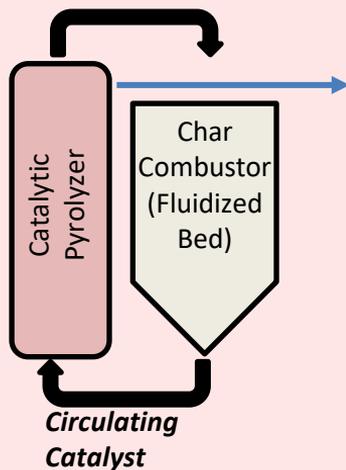
Advantages of the Technology:

- Cost of wood-based feedstock is de-coupled from petroleum price
- Vapor-phase catalytic upgrading provides control over product slate
- Reduces downstream hydrotreating costs as compared to fast pyrolysis
- Upgraded bio-oil could be co-processed in existing refinery infrastructure
- Produces a drop-in fuel blendstock, with co-product opportunities

D. Ruddy, et al. *Green Chem* 16 (2014) 454

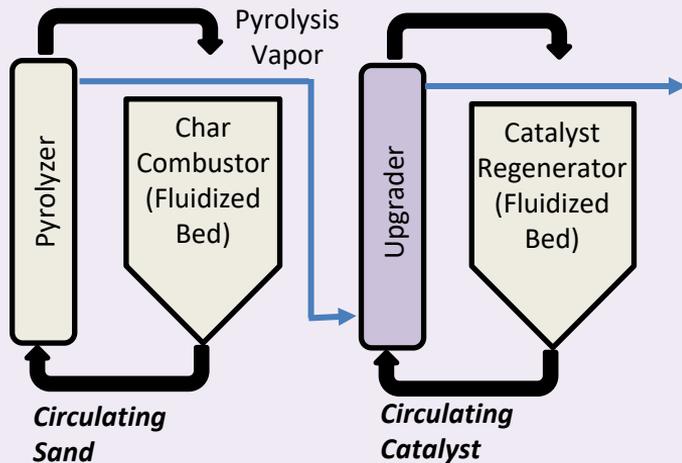
CFP Process Design Options

In-Situ CFP Metal Oxide Catalysts



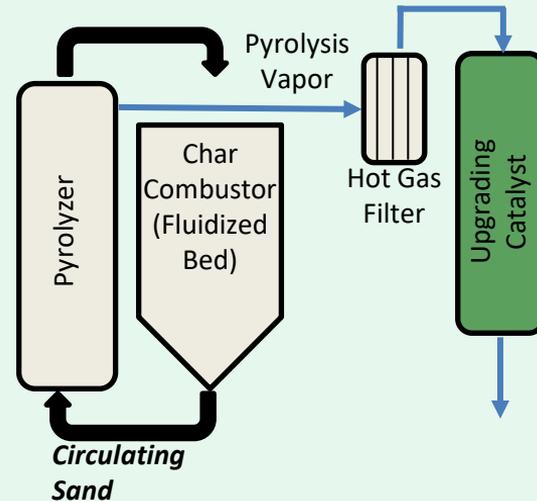
Low capex requirements
Harsh upgrading environment

Ex-Situ Entrained Bed CFP Zeolite Catalysts



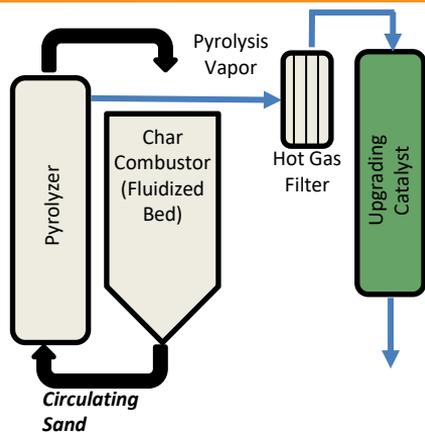
Controlled upgrading environment
Higher capex required

Ex-Situ Fixed Bed CFP Metal-Acid Catalysts



More diverse catalysts and chemistries possible
Longer catalyst lifetimes required

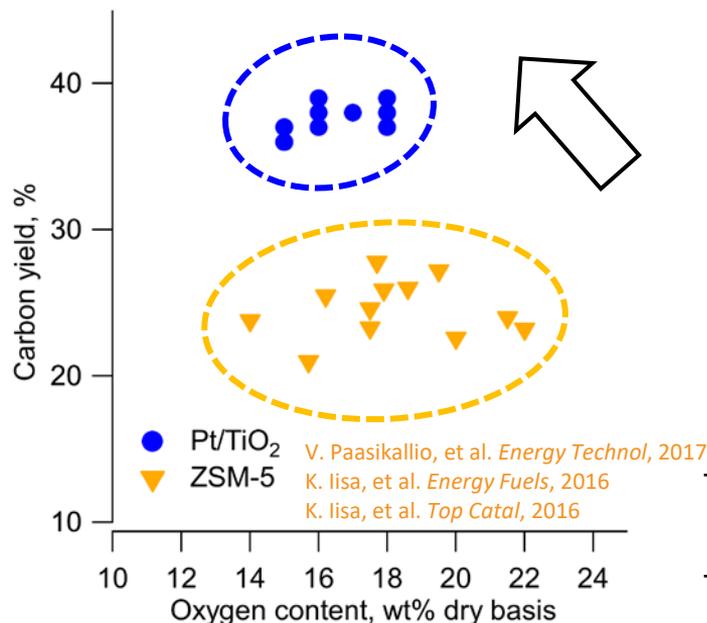
Ex-situ Fixed Bed CFP: 2018 State-of-Technology



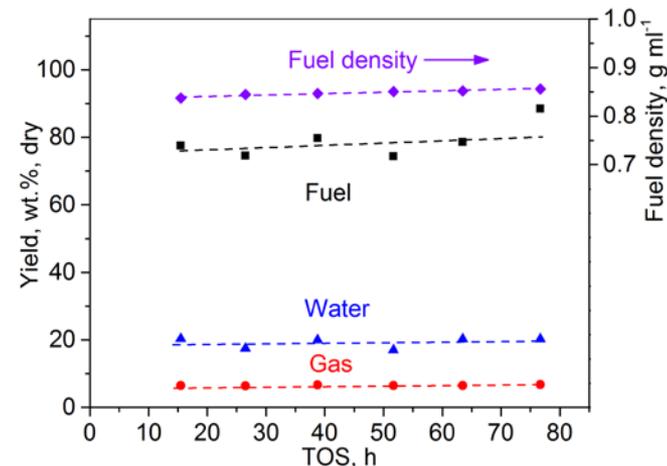
Standard Conditions

Feedstock: Loblolly Pine
 Catalyst: 0.5-2.0 wt% Pt/TiO₂
 Pyrolysis Temperature: 500 °C
 Upgrading Temperature: 435 °C
 Catalyst Mass: 100 g
 WHSV: 1.4 g biomass/gcat*h
 Near Atmospheric Pressure
 Hydrogen Concentration: 83%
 Biomass:Catalyst Ratio: 3-13.2

Improved carbon yields compared to ZSM-5



The Pt/TiO₂ CFP-oil was hydrotreated using a **single stage** system for 80+ hours without fouling or plugging



Carbon yield %	H/C mol/mol	O wt.% dry	Density g ml ⁻¹
89	1.71	0.19	0.851

NiMo Sulfide, LHSV: 0.2-0.3, 13 MPa

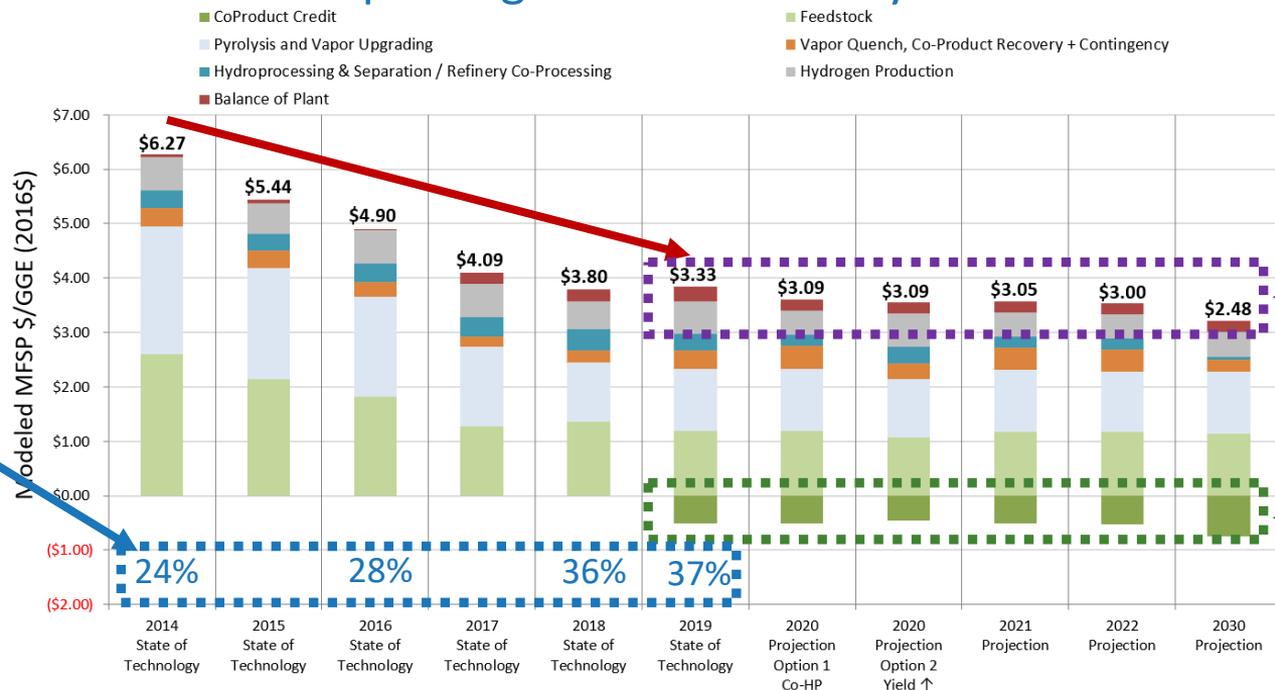
M. Griffin, et al., *Energy Environ. Sci.*, 11 (2018) 2904-2918.

R. French, et al., *ACS Sustain. Chem. Eng.*, 9 (2021) 1235-1245.

Progress on Reducing Biofuel Production Costs from CFP

Reduced modeled biofuel production costs by ca. \$3/GGE since 2014 by improving carbon efficiency

Carbon Efficiency to Fuels and Chemicals



Process Optimization and Durability

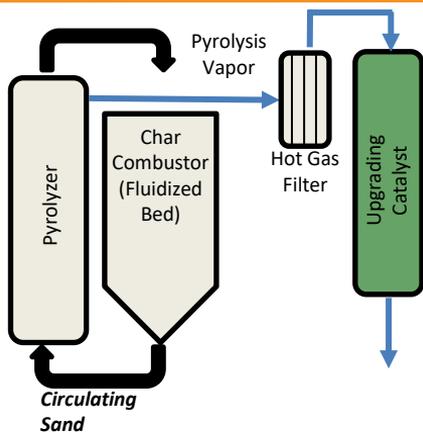
Chemical Co-product Credits

*A. Dutta, et al., 2019 SOT Report, 2020, NREL/TP-5100-76269.

Targeted R&D on process optimization/durability and product diversification

Process Optimization and Durability

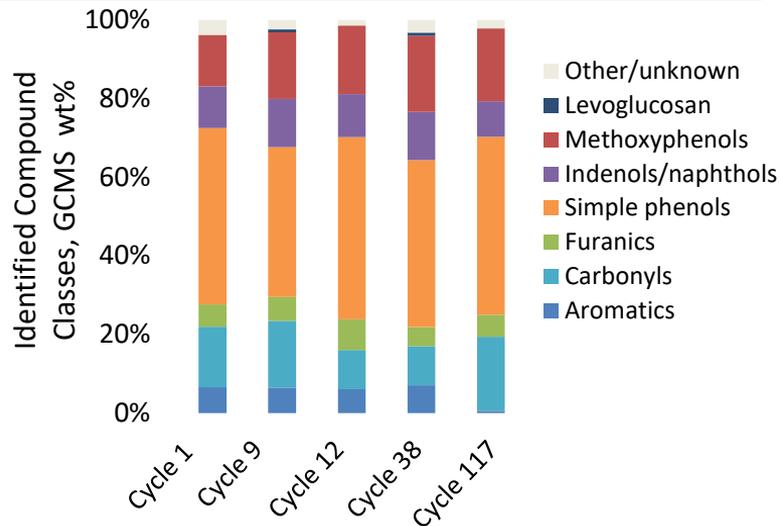
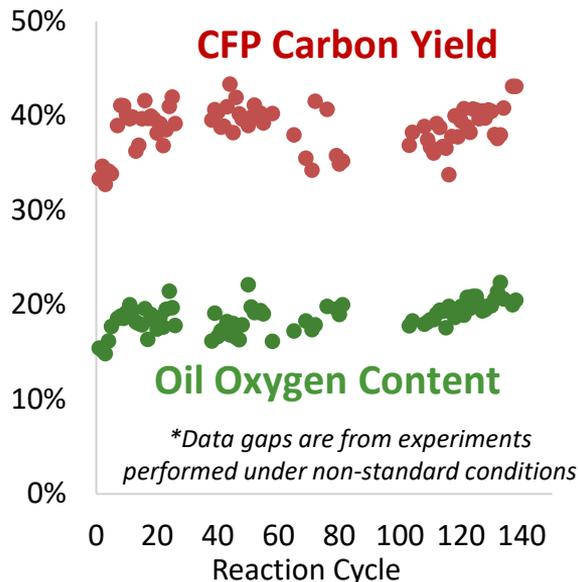
Assessing Process Durability



Standard Conditions

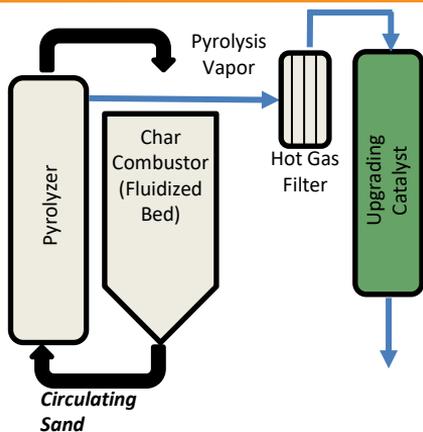
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Upgrading Temperature: 435 °C
Catalyst Mass: 100 g
WHSV: 1.4 g biomass/gcat*h
Near Atmospheric Pressure
Hydrogen Concentration: 83%
Biomass:Catalyst Ratio: 3

Progress: integrated experiments performed for 100+ reaction cycles reveal minimal impact on yields, oil-quality, and product composition



Outcome: improved confidence in catalyst and process durability, reduced risk for process model inputs, and support for technology transfer efforts

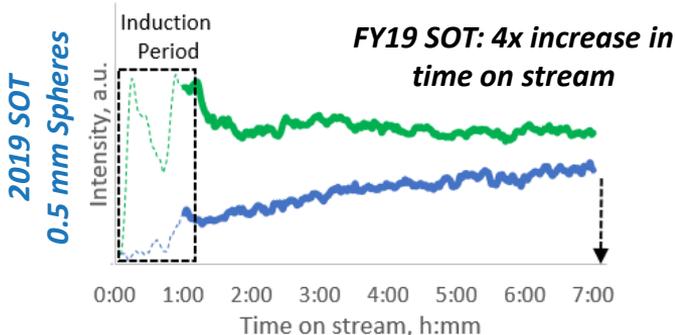
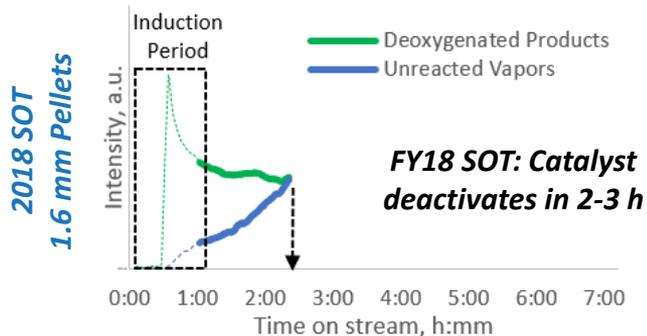
Increasing Cycle Length



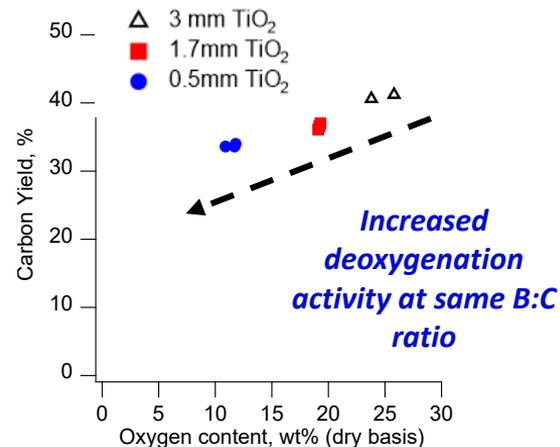
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 Upgrading Temperature: 435 °C
 Catalyst Mass: 100 g
 WHSV: 1.4 g biomass/gcat*h
 Near Atmospheric Pressure
 Hydrogen Concentration: 83%
 Biomass:Catalyst Ratio: 3-12

Progress: optimizing the size and shape of the catalyst support reveals improved deoxygenation activity and increased cycle length



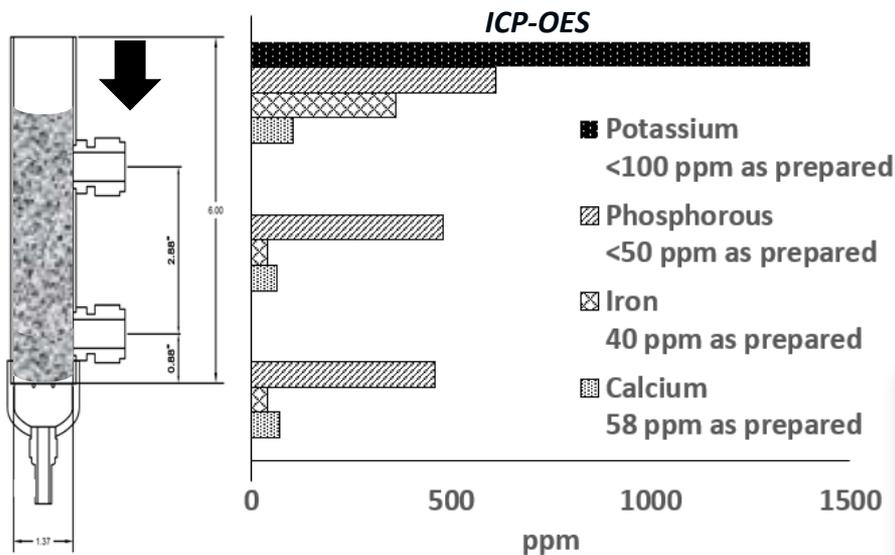
Coke on catalyst reduced from 2.1 wt% to 1.9 wt%



Outcome: lower capital requirements, a **\$0.05/GGE** reduction in MFSP, and improved operational efficiency

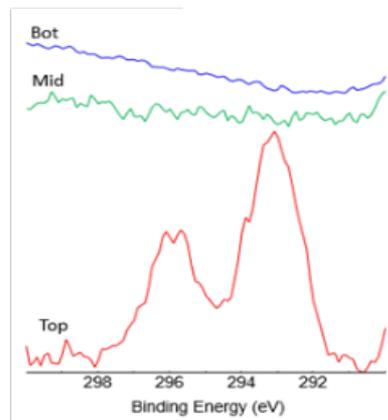
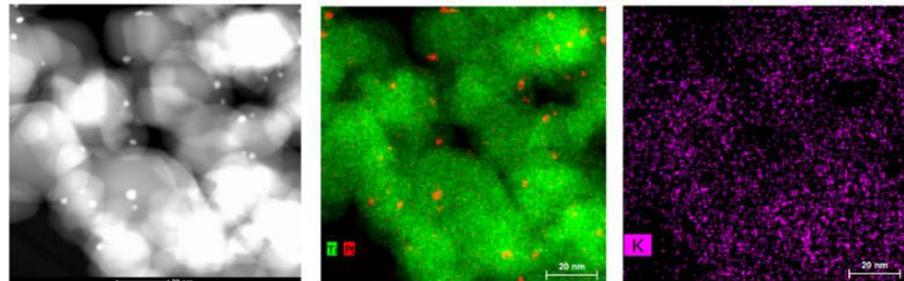
Tracking Inorganic Deposition

Catalyst characterization after reaction with forest residues revealed considerable potassium deposition at the leading edge of the catalyst bed



Experiments performed with a 50:50 wt% blend of clean pine and forest residues for a cumulative time on stream of 32 h

Dark field STEM images and EDS maps indicate well-dispersed K on the surface of the post-reaction samples from the top of the bed



XPS Spectra of K 2p Region confirm K deposition

Ongoing Research:
Determine the impact of K on catalyst properties and performance

Informing Scale Up

Progress: development of a new simulation framework that leverages DOE high performance computing capabilities for multiscale modeling to inform in-silico optimization and process scale up

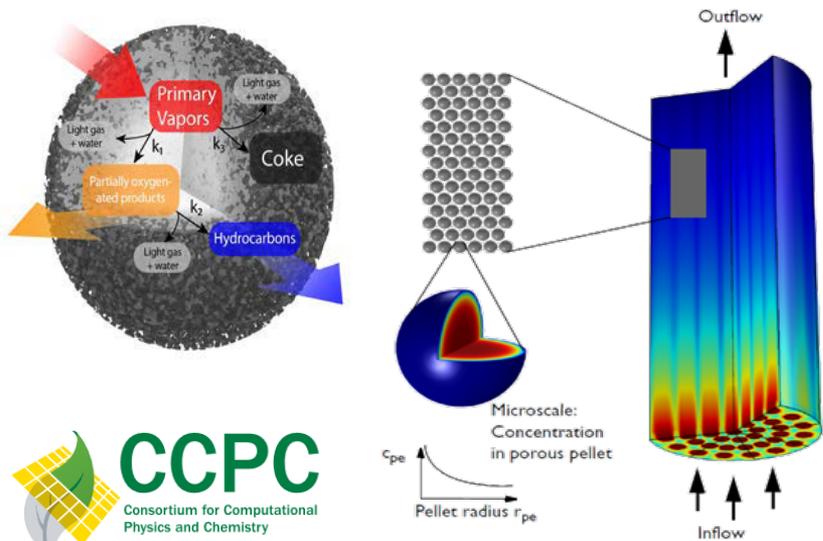
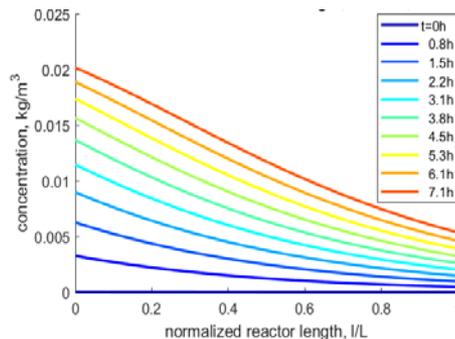
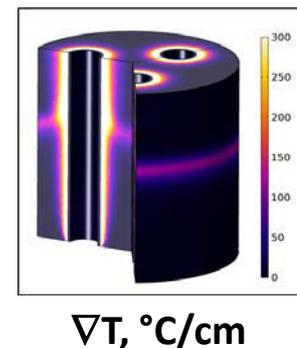


Image made using COMSOL Multiphysics® software and provided courtesy of COMSOL.²⁶

Predicted catalyst coke profile as a function of time on stream



Sharp temperature gradients during regeneration at pilot-scale



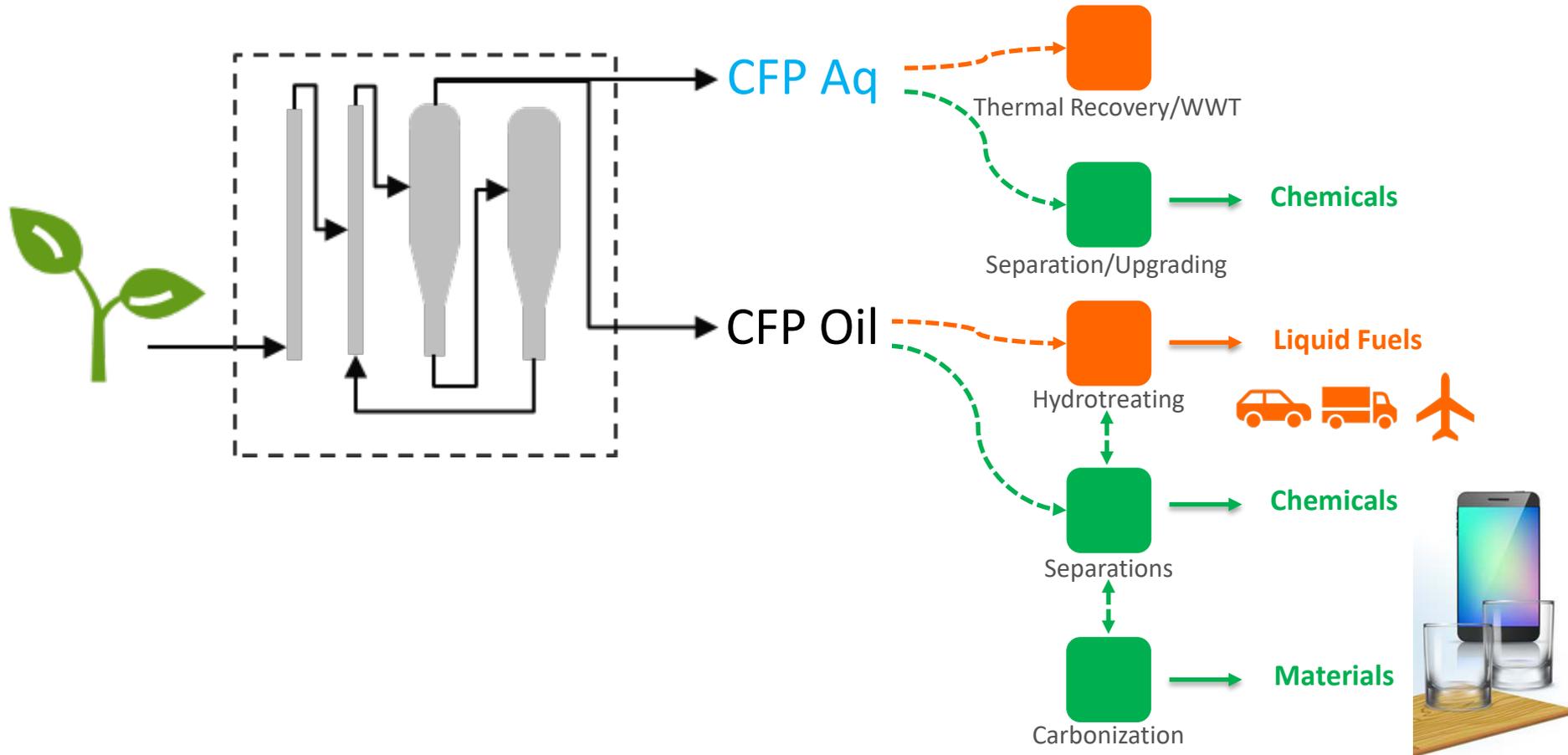
Outcome: early identification of potential process disruption at the pilot scale due to thermal excursions during regeneration. Ongoing collaborative research targets alternative reactor designs to improve heat transfer capabilities at scale

B. Pecha, et al., *Reaction Chemistry and Engineering*, 6 (2021) 125-137.

B. Adkins, et al., *Reaction Chemistry and Engineering*, (2021) in press

Product Diversification

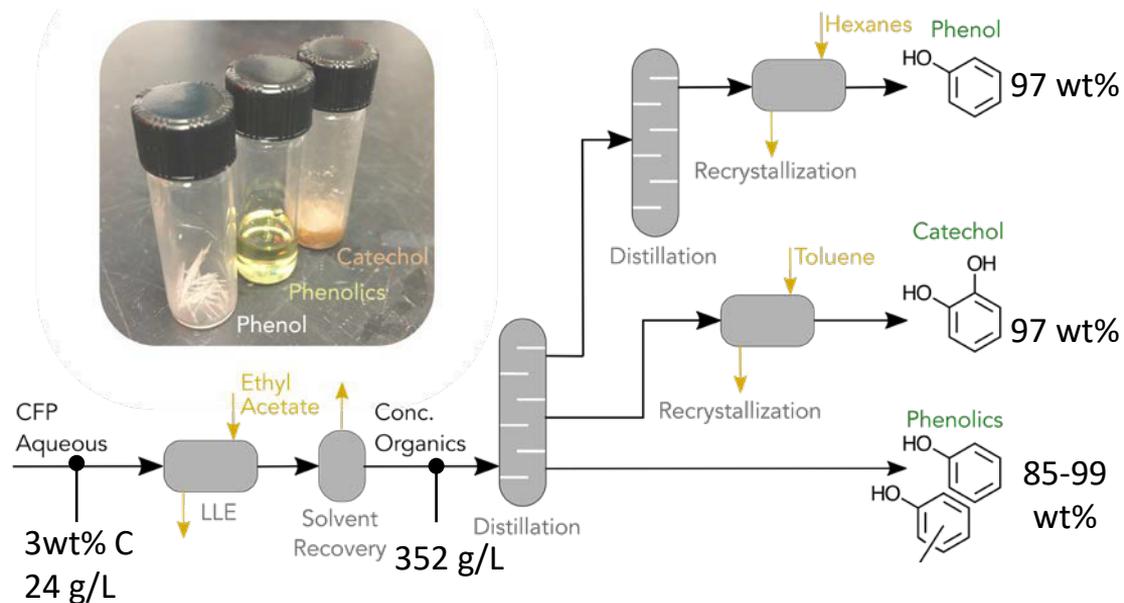
Expanding the Product Slate from CFP



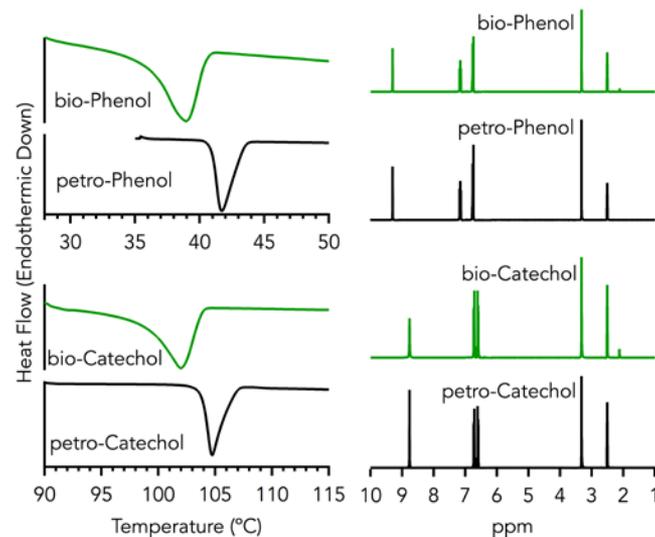
Valorizing the CFP Aqueous Waste Stream

Expanding product slate from CFP technology platform by developing separation strategies for chemical precursors

Separations Approach



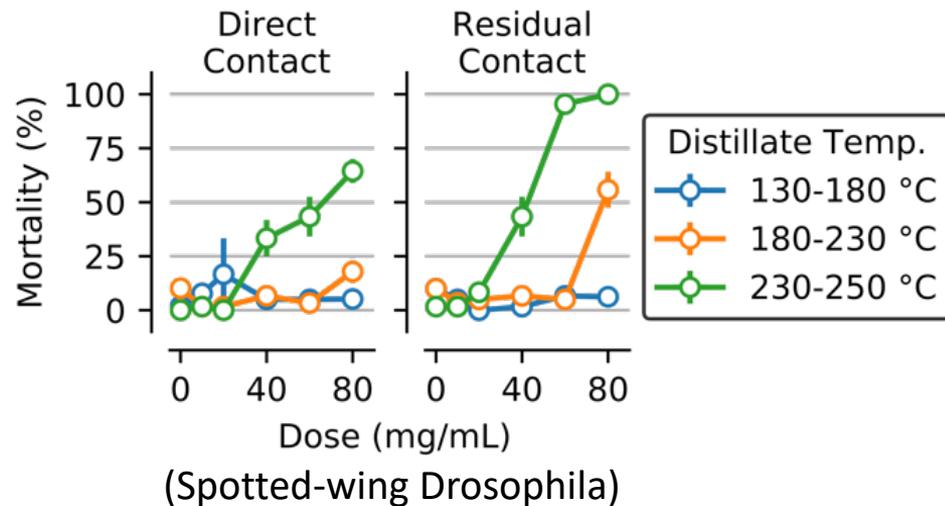
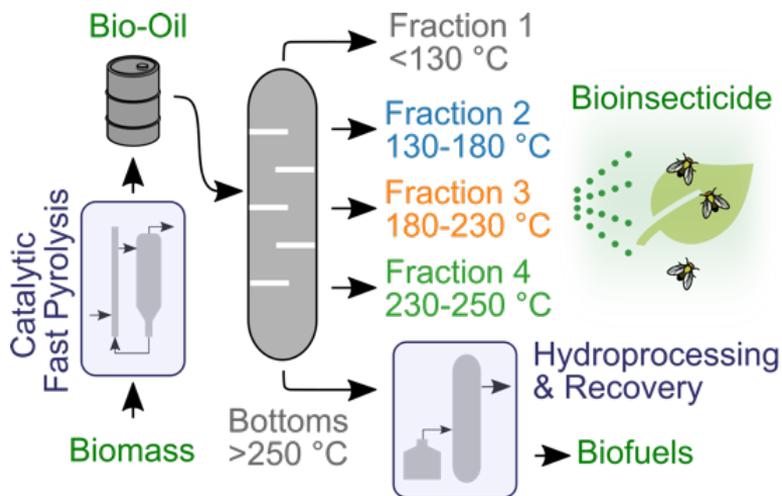
Product Characterization



A. N. Wilson, et al., *Green Chemistry*, 21 (2019) 4217-4230

Bioinsecticides derived from CFP Bio-Oil

Fractions of CFP bio-oil exhibit activity as bioinsecticides, presenting an opportunity to improve sustainability in energy and food production sectors



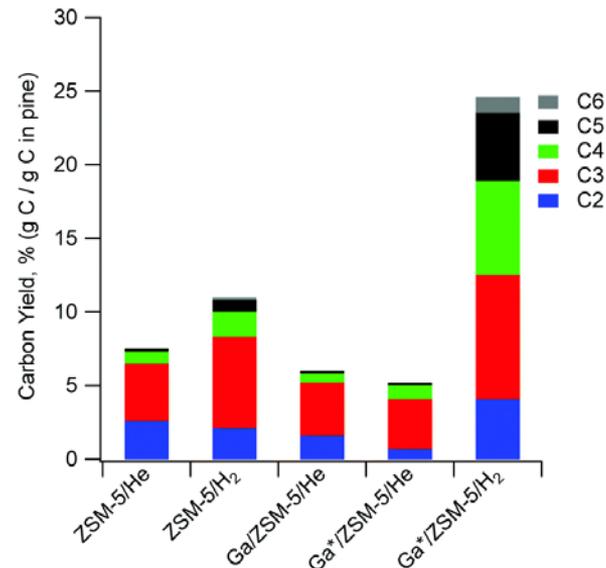
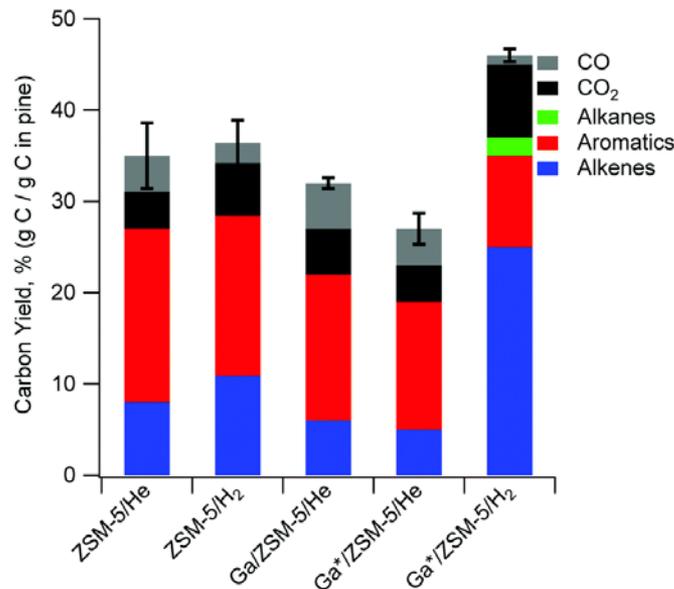
Extent of phenol alkylation appears to be correlated with mortality



Targeting Olefins as Primary CFP Products

Early-stage results suggest that modifying the catalyst and process conditions enables the CFP product slate to be tuned towards olefins

- Feedstock: Southern yellow pine
- Pyrolysis and catalysis temperature: 500°C
- Apparatus: Tandem micro-furnace pyrolyzer coupled to a GC-MS/FID
- Pressure: 115kPa
- B/C: 0.05
- Run in triplicate



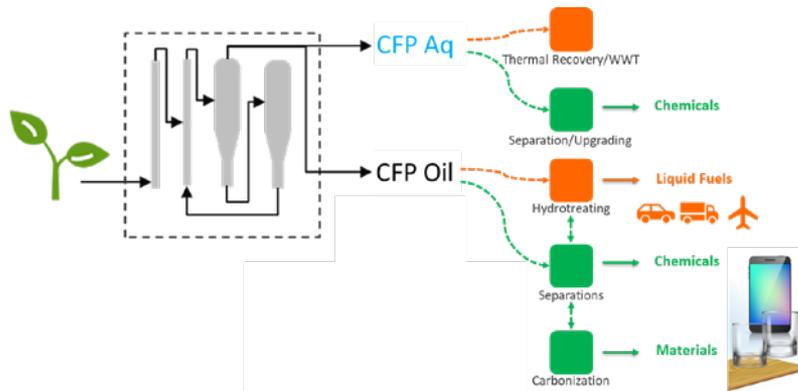
Ga* indicates Ga/ZSM-5 pretreated in H₂

Reduced Ga species (e.g., [Ga(OH)₂]⁺ and [GaH(OH)]⁺) appear to be responsible for improved olefin yield

K. Lisa, et al., *Green Chemistry*, 22 (2020) 2403-2418

Summary and Conclusions

- **Designed resilience as a central theme** for emerging carbon conversion and management technologies
- **Critical Needs:**
 - Feedstock flexibility
 - Adaptive process design and control
 - Low conversion costs
 - Product tunability
- **Catalysis enables the development of versatile technology platforms** that meet these needs



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Thank you!



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