



Catalytic Upgrading of Biomass Pyrolysis Vapors at Bench Scale with Pt/TiO₂

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Overview

- Status of and motivations for upgrading biomass pyrolysis vapors to fuel intermediates with Pt/TiO₂ and H₂
- Progress in reducing process cost
 - Reducing catalyst cost
 - Reducing regeneration time
 - Varying upgrading parameters
 - Catalyst lifetime
 - Changing pyrolysis temperature
- Constraints
 - Not increase oxygen in oil
 - Not increase hydrotreating requirements
 - Not decrease yield

Why Pt/TiO₂ catalytic fast pyrolysis and hydrotreating?

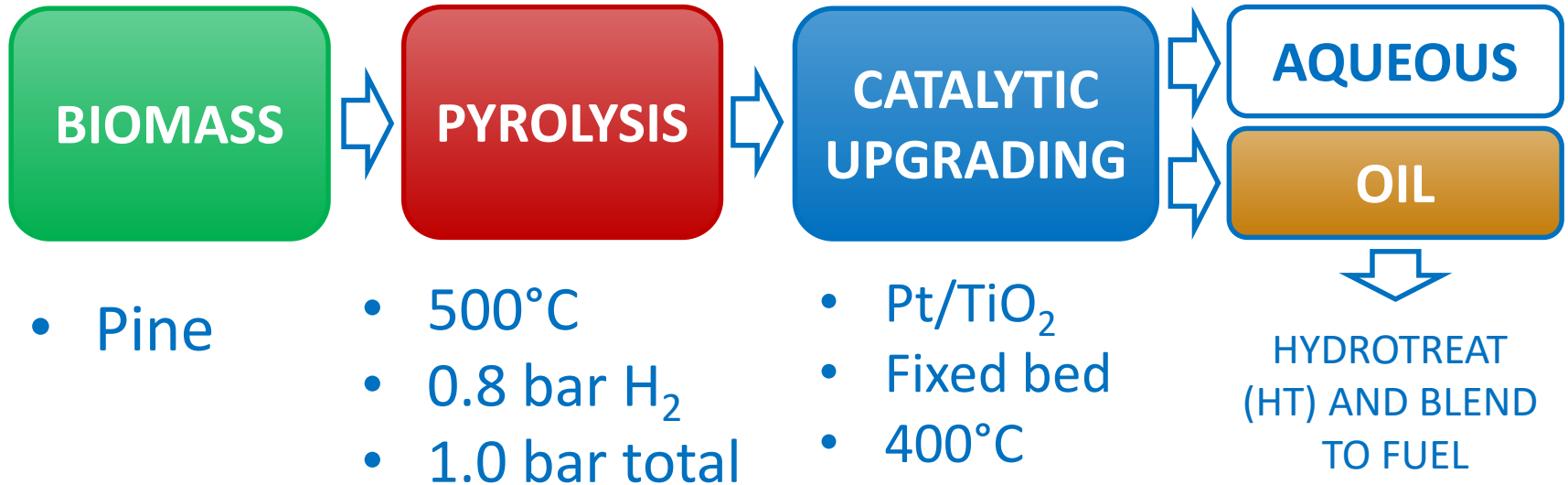
- Monday talk (C. Mukarakate, “Performance Comparison of three Biomass Catalytic Fast Pyrolysis Pathways...”) and Griffin et al. paper (below)
 - Hydrotreating (HT) of Catalytic fast pyrolysis oils (CFP) is lower cost and more reliable** than hydrotreating of raw pyrolysis oil
 - CFP with Pt/TiO₂ and hydrogen gives higher yield (and carbon yield) than ZSM-5 upgrading**
 - Some HDO of oxygenates means less carbon lost as CO_x
 - Hydrogenation of coke precursors reduces carbon lost to coke

	Carbon Yield	Oxygen content
¹ Pt/TiO ₂	38%	16%
² HZSM5	24%	22%

1. Griffin et al. E&ES, 2018, DOI: 10.1039/c8ee01872c
2. Paasikallio et al. Grn. Chem. 2014, 16, 3549

CFP process

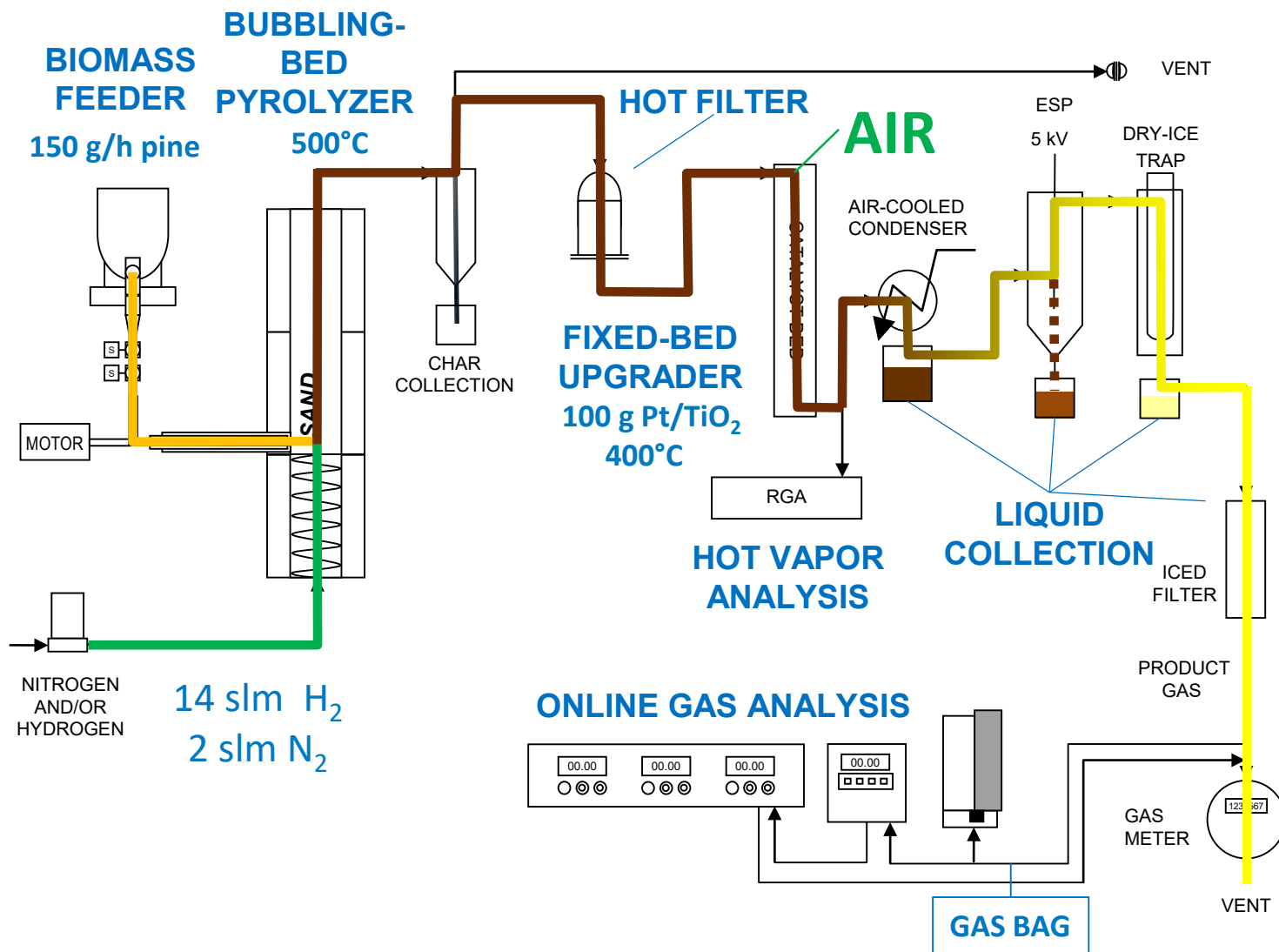
• OIL PRODUCTION



• REGENERATION OF FIXED-BED CATALYST



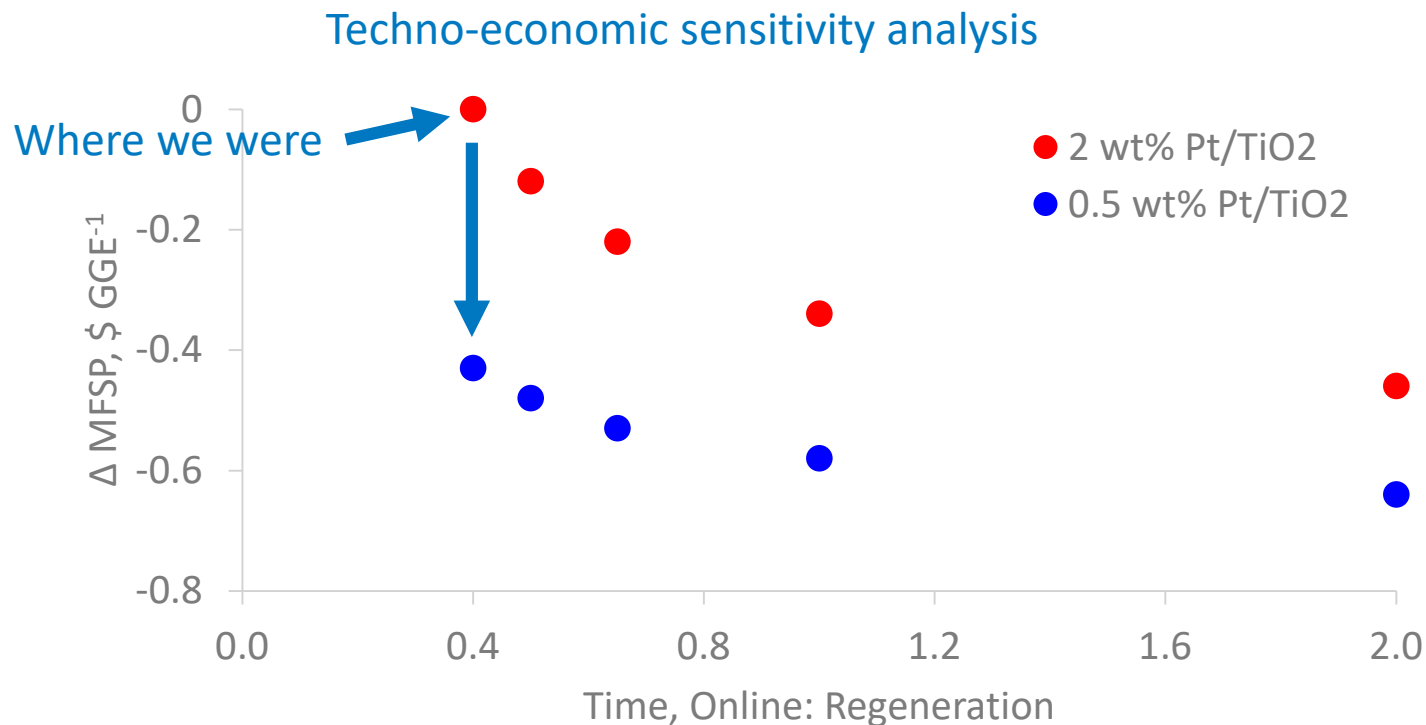
Experimental System



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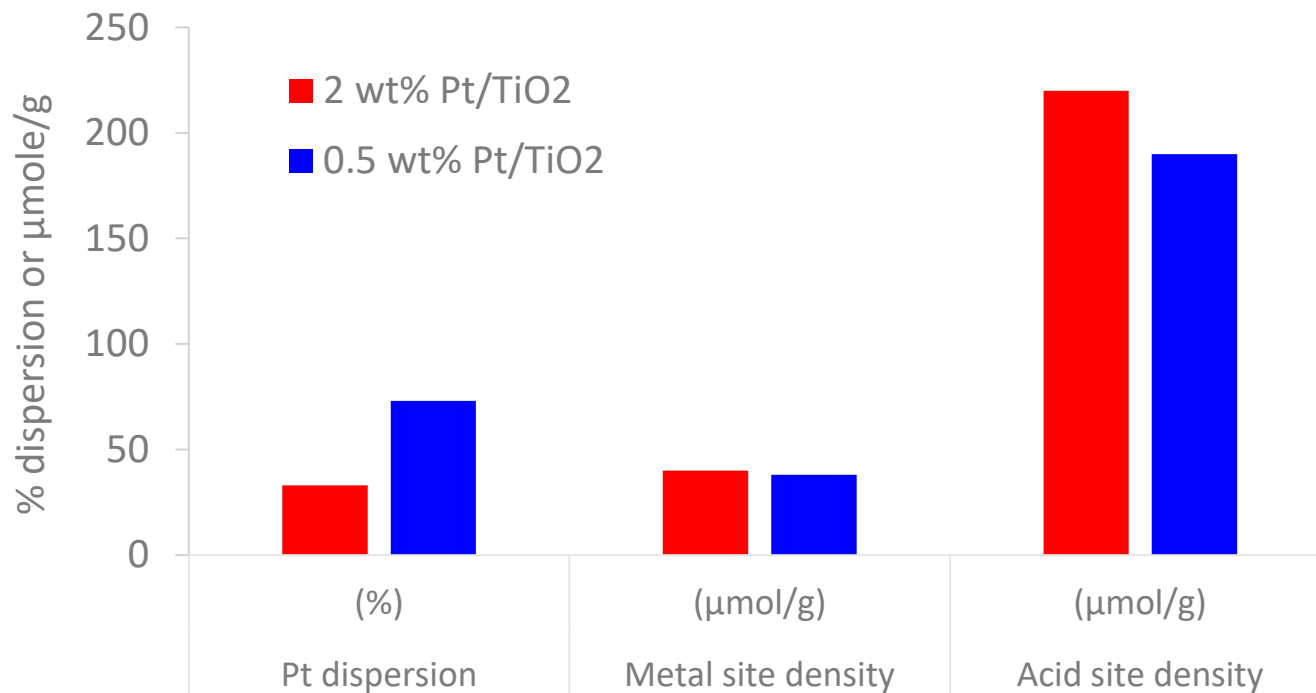
Process cost is sensitive to catalyst cost



- Need to decrease platinum while maintaining performance

Adapted from Griffin et al. E&ES, 2018, DOI: 10.1039/c8ee01872c

Can a lower Pt (cost) catalyst work? Catalyst properties



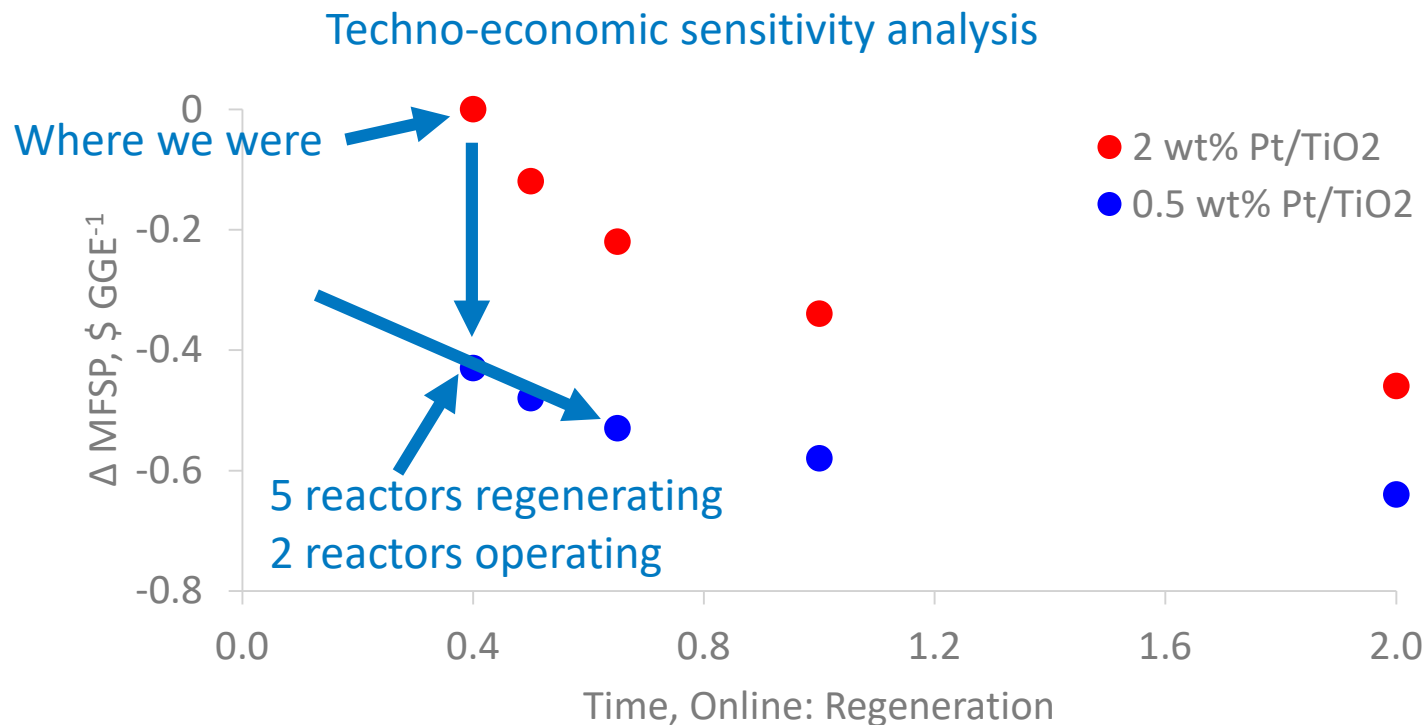
- 2% Pt made by incipient wetness
- 0.5% Pt by strong electrostatic adsorption (SEA)
- Higher dispersion of Pt on 0.5% makes properties of two catalysts very similar

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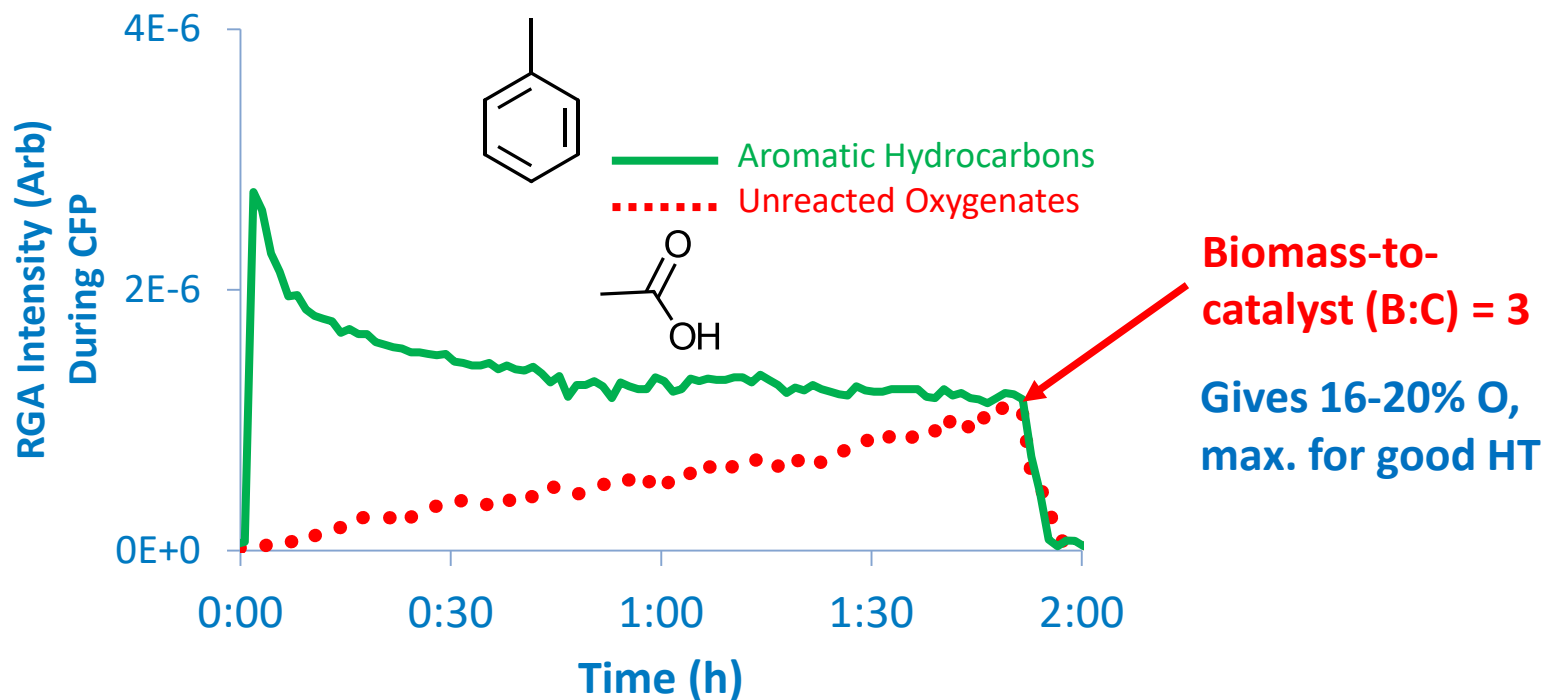
Process cost is sensitive to regeneration time



- Increasing online : regeneration time reduces number of reactors and catalyst inventory

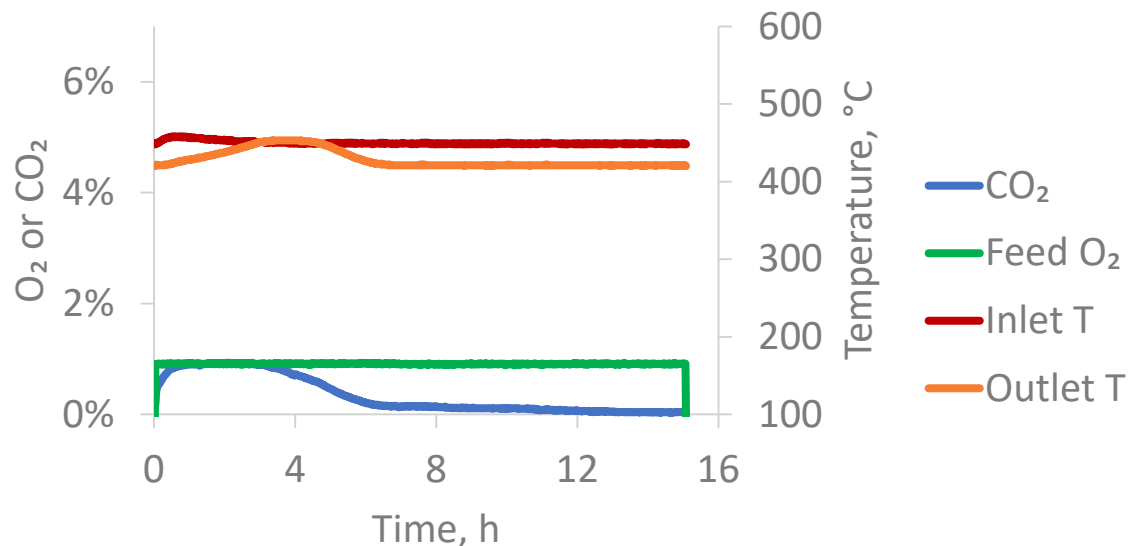
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When is regeneration necessary?



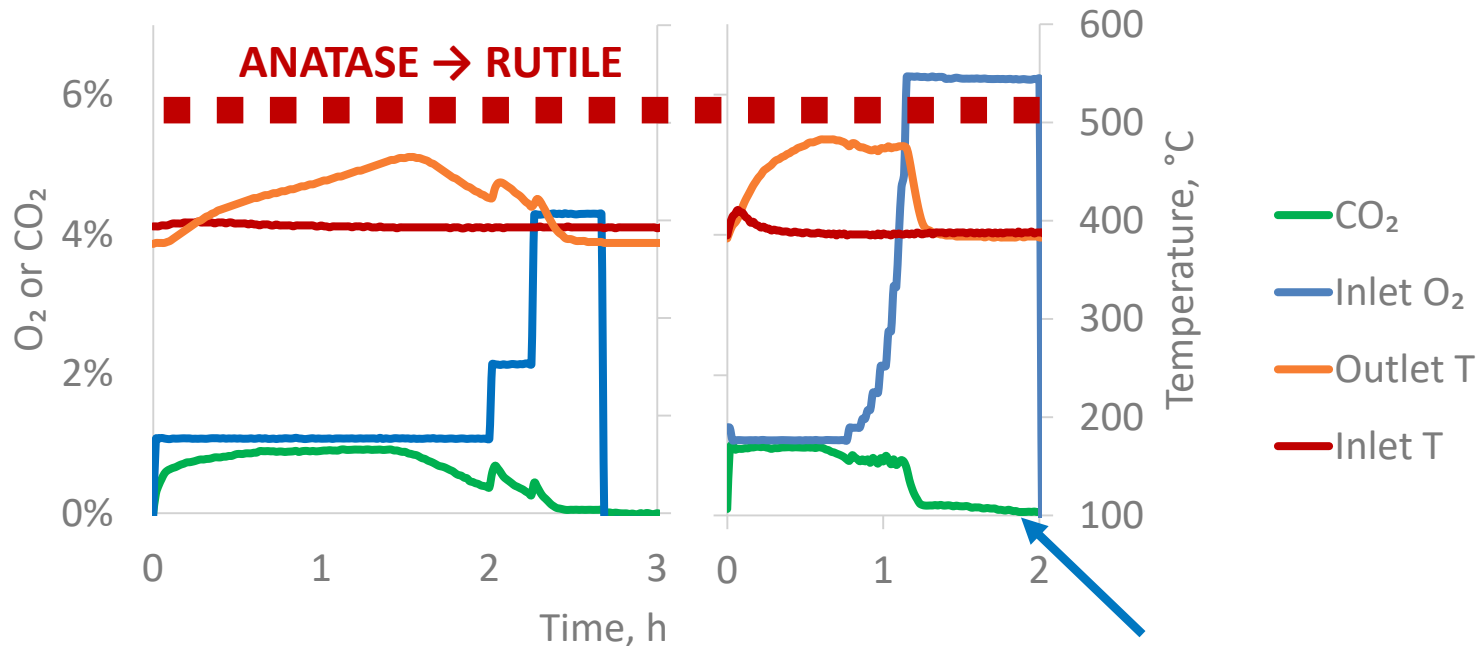
Regeneration Protocols

- Remove coke → oxidize in O₂/N₂ mixture
 - overnight in 1% O₂/99% N₂ at 450°C



- Reactivate catalyst → treat in H₂
 - 2+ h with 85% H₂/15% N₂
- Overall 17 h

Shorter regenerations achieved

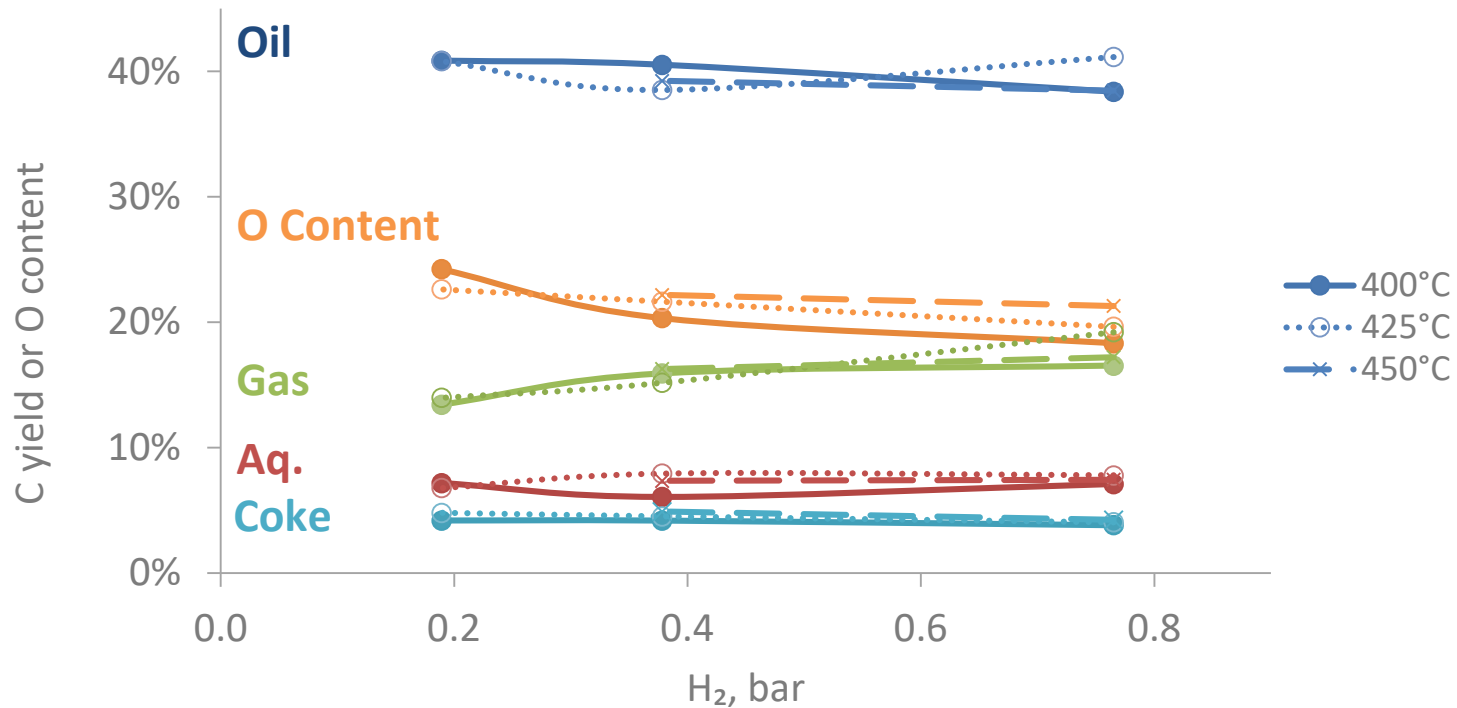


- Catalyst oxidation shown above
- Also, Reduction time reduced to ~1h in 85% H₂
- Online: regeneration 2:3 (0.66)

Overview

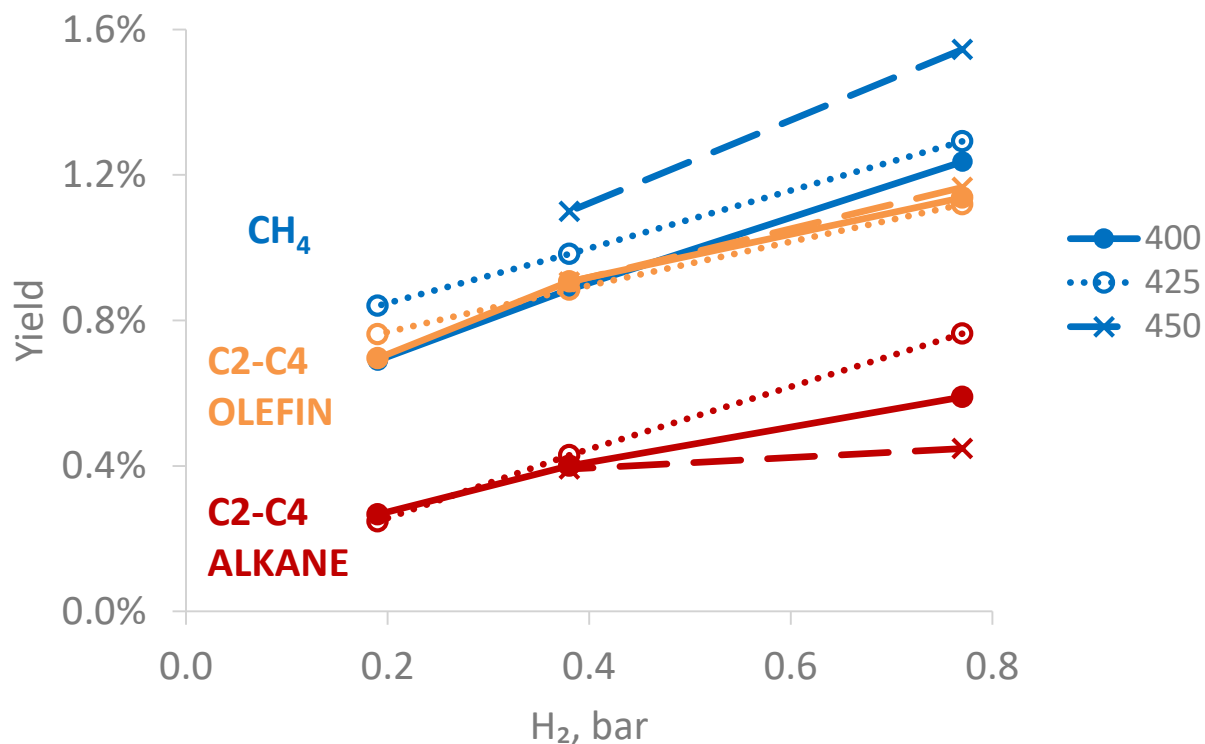
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Varying hydrogen partial pressure and catalyst temp.



- Temperature effects are not significant
- Increasing hydrogen partial pressure
 - Decreases oil oxygen content
 - Increases gas yield
 - Enhances hydrodeoxygenation

Impact of H₂ Partial Pressure on Gas Yields

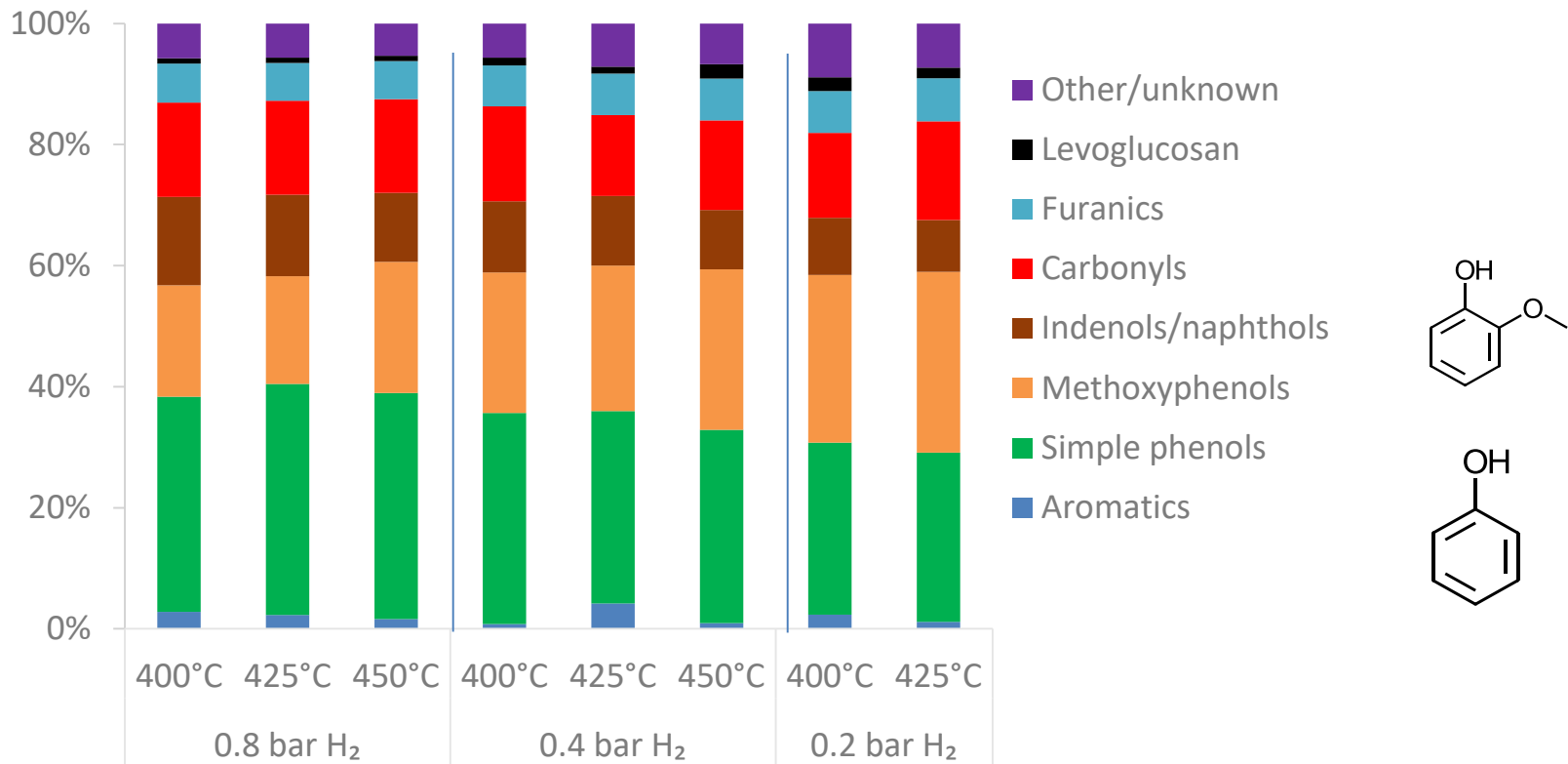


Increasing H₂ partial pressure

- Increases CH₄ and light alkane and alkene formation (increased cracking)
- Increases aqueous mass yield

Consistent with increased hydrodeoxygenation (HDO)

GC/MS composition changes with H₂ partial pressure & T_{cat}

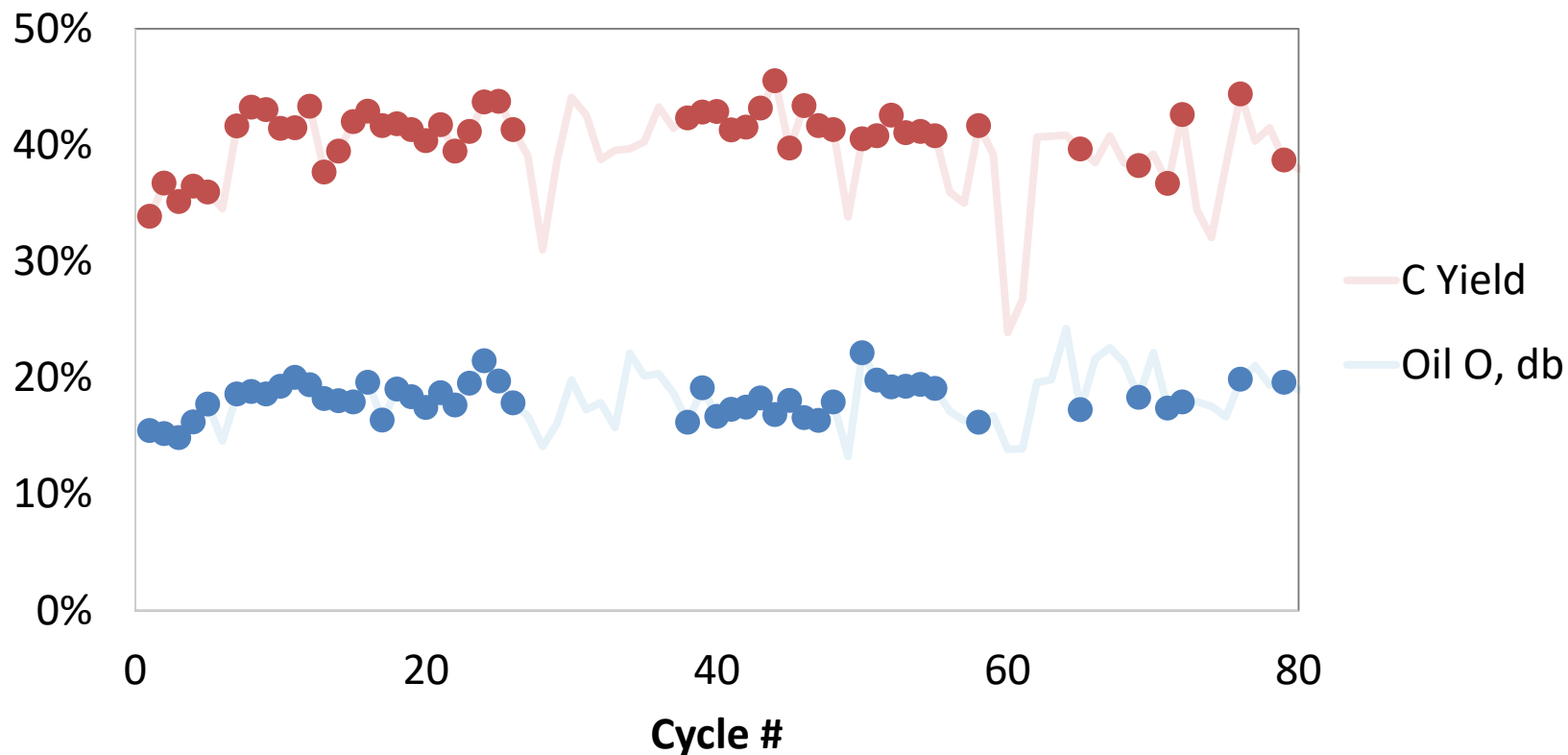


- As H₂ decreases, more methoxyphenols, less alkylphenol/phenol

Overview

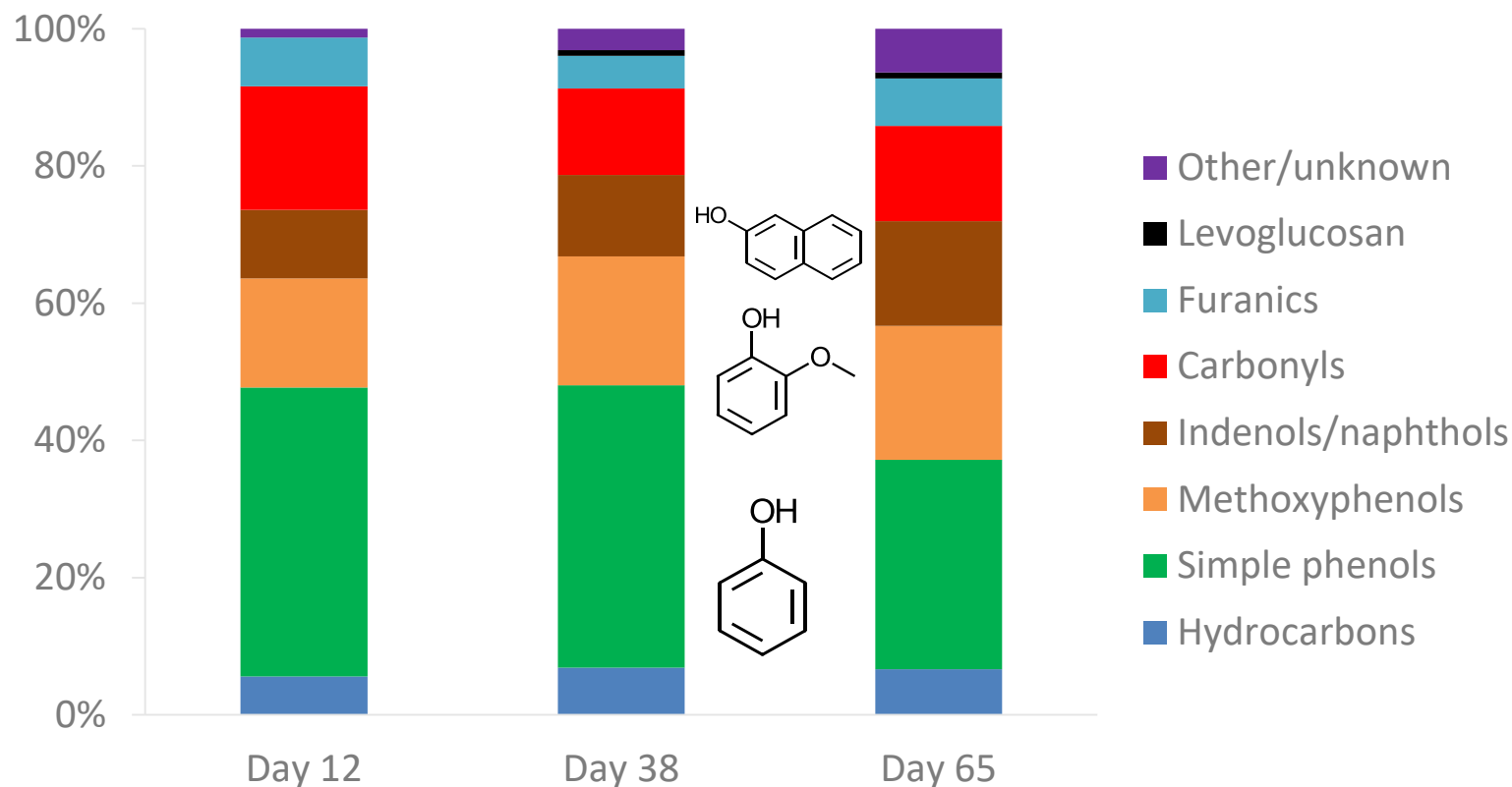
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Catalyst stable past 150 hours



- Highlighted points are Pine/500C/400C/0.8 bar H₂/ B:C = 3
- Each cycle is 2 h
- Stable after initial break-in

Only slight variations in composition with catalyst aging

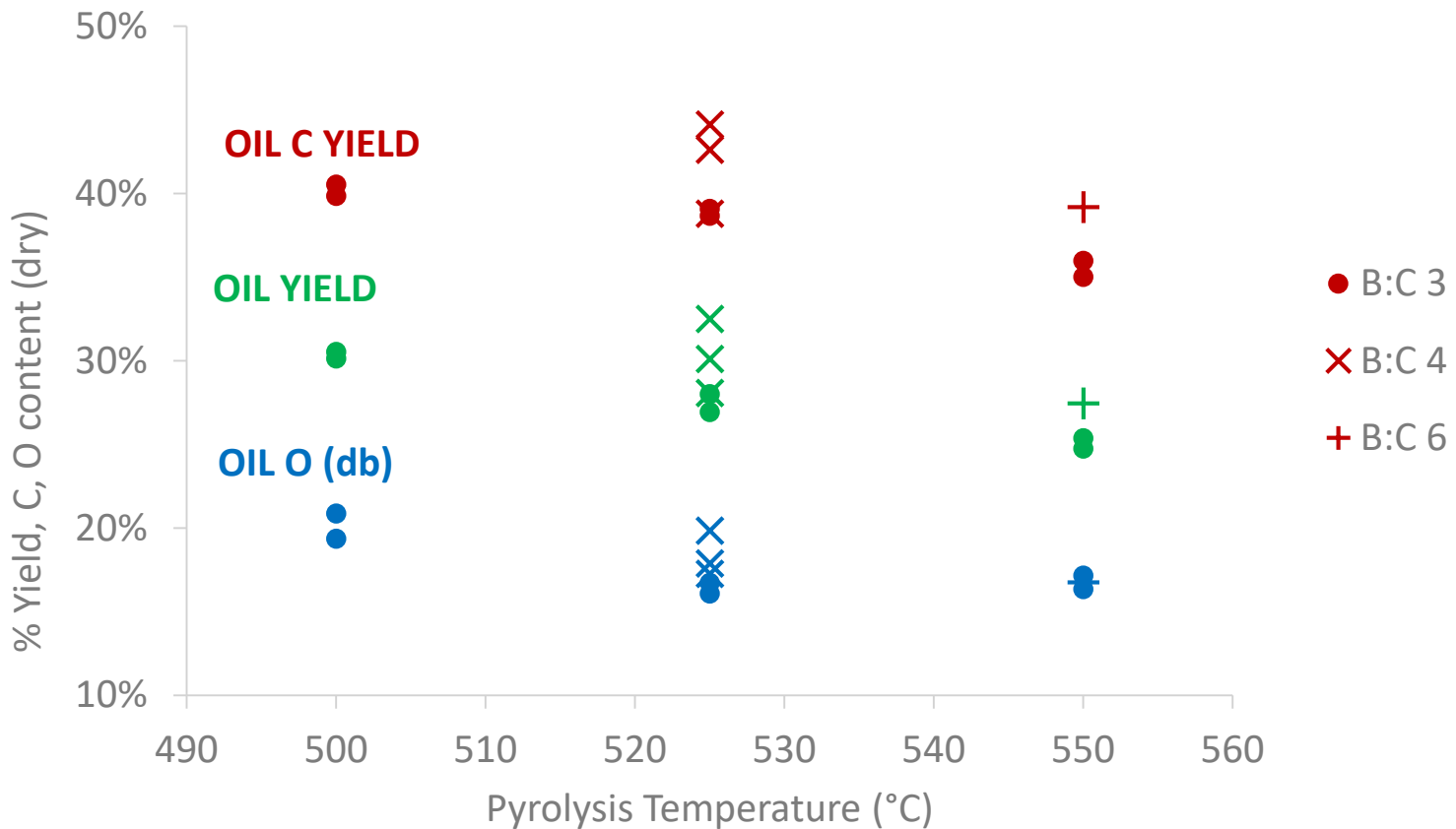


- Slight decrease in phenols, increase in methoxyphenols and naphthols

Overview

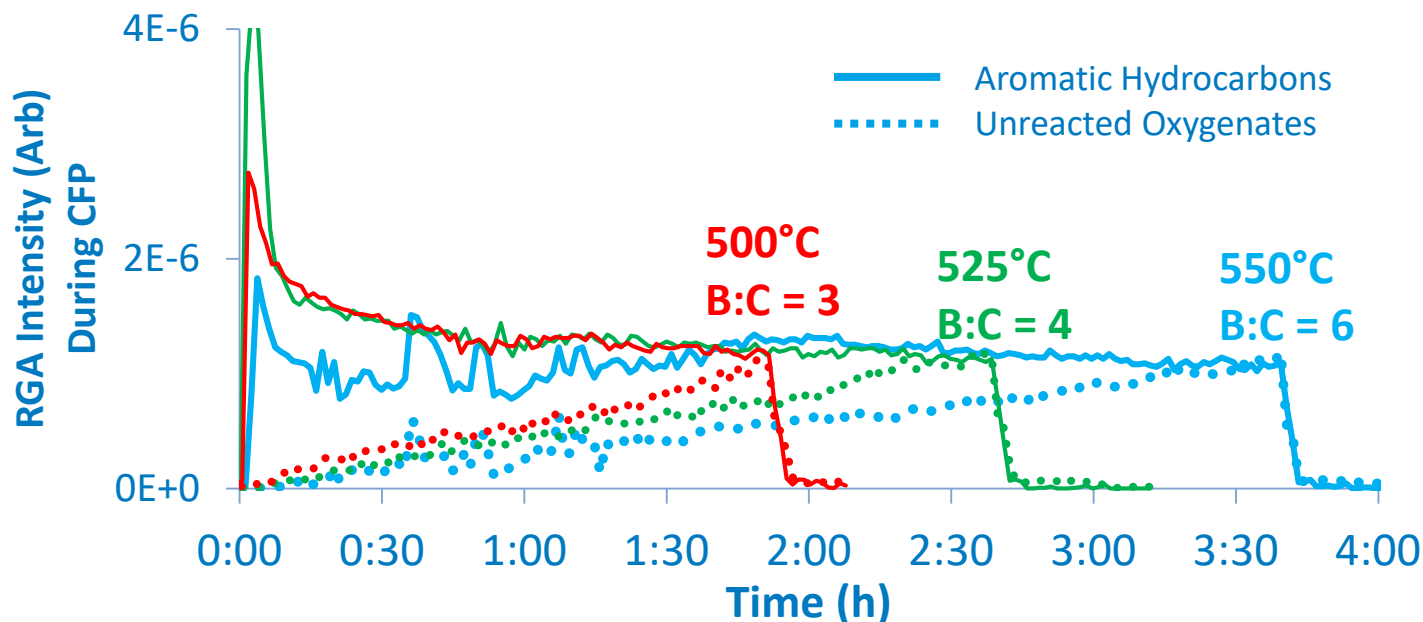
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Higher pyrolysis temperature gives higher B:C at low O



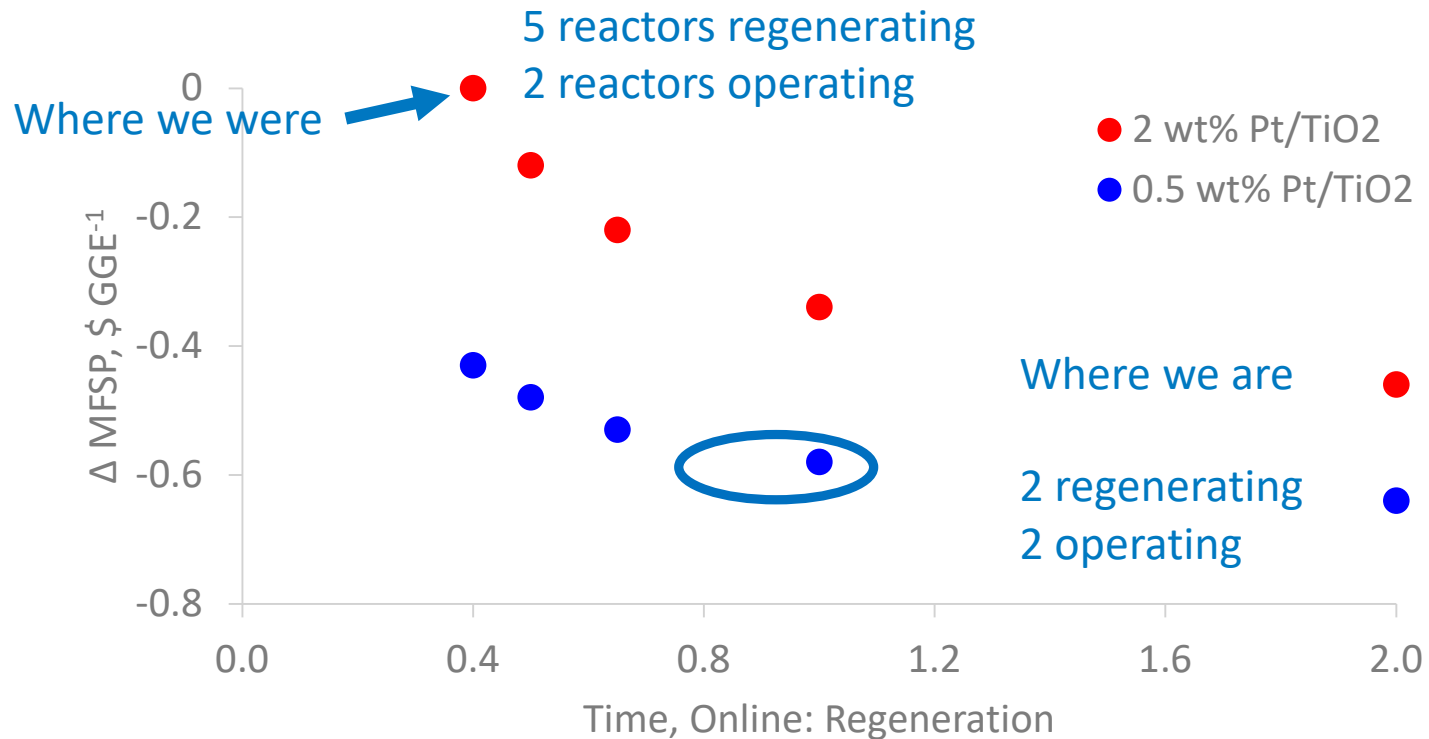
- Potential for even higher biomass: catalyst than shown

Higher pyrolysis temperature delays breakthrough



- Delayed onset of unreacted oxygenates
- Gives onstream: regeneration time of 0.75-1.1 by giving longer onstream time

Summary: How much progress have we made?



- Have improved cost substantially

Adapted from Griffin et al. E&ES, 2018, DOI: 10.1039/c8ee01872c

Conclusions & Future

- Conclusions
 - Lower-Pt catalyst performs comparably to higher-Pt catalyst
 - Regeneration shortening improves projected cycle time
 - Increasing hydrogen pressure decreases oxygen and methoxyphenols, increases phenols
 - Increasing pyrolysis temperature 500-550°C delays catalyst deactivation while giving comparable yield and oxygen, increasing time-on-stream
- Future:
 - Decrease catalyst cost
 - Higher B:C through higher pyrolysis temperature
 - Identify bad actors in pyrolysis oil
 - Lower-cost feedstock

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Questions?

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