INTRODUCTION

A number of factors are currently converging to compel significant changes in automobile spark-ignition (SI) fuel and engine technology. Concerns regarding global climate change caused by greenhouse gas emissions [1] are leading to legislation in many countries mandating the use of low-net carbon emission fuels, primarily biofuels [2]. In the United States, for example, renewable fuel usage is mandated to increase under the Renewable Fuel Standard [3]. The same climate change concerns are driving the introduction of more stringent standards for fuel economy as well as greenhouse gas emissions at the tailpipe [4]; this in turn is driving research to increase the efficiency of SI engines. High-efficiency SI engines will apply a number of different technologies, including direct injection (DI), which takes advantage of evaporative cooling of the intake charge to reduce engine knock, allowing an increase in boost pressure and/or compression ratio [5]. Further increases in boost pressure and compression ratio (and consequently efficiency) require use of more highly knock-resistant fuel to maintain optimal or near optimal combustion phasing.

The ability of an SI engine fuel to resist autoignition and avoid knock is measured as octane number, a critical performance parameter for SI engines. In the United States, the octane number used for retail gasoline is the anti-knock index, which is the average of the research octane number (RON) (ASTM D2699-13b) and motor octane number (MON) (ASTM D2700-13b). The primary differences between the RON and MON measurements are intake charge temperature and engine speed, with the RON test using a significantly lower (and variable) intake charge temperature and 600 revolutions per minute (rpm) engine speed, while the MON test is conducted at a much higher, fixed intake charge temperature and 900 rpm engine speed. Relevant gasoline properties including research octane number (RON), motor octane number, distillation curve, and vapor pressure were measured. Detailed hydrocarbon analysis was used to estimate heat of vaporization and particulate matter index (PMI). Experiments were conducted to measure knock-limited spark advance and particulate matter (PM) emissions. The results show a range of knock resistances that correlate well with RON. Molecules with relatively low boiling point and high vapor pressure had little effect on PM emissions. In contrast, the aromatic oxygenates caused significant increases in PM emissions (factors of 2 to 5) relative to the base gasoline. Thus, any effect of their oxygen atom on increasing local air-fuel ratio was outweighed by their low vapor pressure and high double-bond equivalent values. For most fuels and oxygenate blend components, PMI was a good predictor of PM emissions. However, the high boiling point, low vapor pressure oxygenates 2-phenylethanol and 2,4-xylenol produced lower PM emissions than predicted by PMI. This was likely because they did not fully evaporate and combust, and instead were swept into the lube oil.

where $K$ is a function of the temperature-pressure history that the fuel-air mixture experiences in the engine and is therefore different at different engine operating conditions. However, for specifying knock resistance in terms of OI, values of $K$ at the most knock-limited low-speed, high-load conditions are most relevant. In boosted direct-injection spark-ignition (DISI) engines at low speed and high load, $K$ is negative, consistent with the fact that fuels with higher octane sensitivity give higher knock resistance [10].

DISI engines can show substantially higher particulate matter (PM) emissions, on both a mass and particle number (PN) basis, compared to earlier technology port fuel injection engines [11, 12, 13, 14]. Because of the negative health impacts of fine particles [15] and the contribution of soot particles to global warming [16] regulatory agencies are putting in place large reductions in allowable levels of PM emissions for future model years [17, 18, 19]. Increased PM emissions from DISI engines are caused by diffusion combustion in locally rich regions. This can occur because of incomplete fuel spray breakup and evaporation, as well as impingement of the fuel spray on the piston or cylinder wall, and is made worse if substantial amounts of low volatility components are present in the fuel. Combustion then occurs as a diffusion flame or pool fire as the fuel evaporates with consequent production of soot [20,21].

For three-way catalyst equipped cars, the particles emitted at the tailpipe are 95% elemental carbon and consist almost entirely of accumulation mode particles (>30 nm) with an average diameter of about 70 nm [22,23]. It has also been noted that much higher levels of particles are generated during acceleration and cold-start operation as compared to steady-state. Therefore, for vehicle emission regulatory purposes steady-state test cycles are not appropriate. However, Aikawa and coworkers show very similar trends in fuel effects on PM emissions for transient and steady-state vehicle driving cycles [13]. Researchers at Honda have shown that for both port fuel injection and DI engines PM emissions are correlated with a particulate matter index (PMI) that can be calculated based on a detailed hydrocarbon analysis (DHA) for a gasoline. PMI is a function of the weight fraction, vapor pressure, and double bond equivalent (DBE) value for each component in the fuel [13,20]. Fuel components with high vapor pressure will evaporate quickly, minimizing diffusive, heterogeneous combustion or avoiding pool fire combustion if piston impingement occurs. The DBE is the number of hydrogen molecules required to saturate the double bonds and open rings present in a fuel molecule. A global survey of 1,445 gasoline samples showed a PMI range of 0.67 to 3.86 with a mean of approximately 1.6. A typical U.S. certification gasoline exhibits a PMI of 1.36 [13].

Ethanol produced from starch is the primary renewable fuel used in SI engines today, and ethanol may have several distinct advantages for application in DISI engines [24,25]. To achieve much larger quantities of biofuel with lower life-cycle greenhouse gas emissions, production must shift to lignocellulosic biomass feedstocks [26], which can be economically converted to ethanol [27]. Nevertheless ethanol is not without its disadvantages, including low volumetric energy content, high water solubility, and potential materials compatibility issues at high blend levels, all of which prevent it from being considered as a drop-in fuel. Thus, a large international research effort is focused on converting lignocellulosic biomass into drop-in fuels, which are conventionally thought to be hydrocarbons. However, biomass typically contains 40 percent by weight (wt%) to 60 wt% oxygen, suggesting that conversion to hydrocarbons will be both technically and economically challenging. Analysis has shown that costs for hydrotreating of pyrolysis oil derived from biomass can exceed $1 per gallon, with particularly high incremental costs for removal of the last increment of oxygen [28,29]. Gasoline boiling range oxygenates from partially upgraded biomass pyrolysis oils or made from biomass by acid or base-catalyzed deconstruction include phenolics, aryl ethers, and furans [30, 31, 32, 33, 34]. Additionally, isobutanol can be produced by fermentation of sugars, including cellulose-derived sugars [35]. Many of these oxygenates have high octane numbers and high energy density [36] and are thus desirable for enabling the deployment of more efficient DISI engines. The study reported here is part of an effort to determine the extent to which biomass oxygenates can function as drop-in fuels. We specifically focus on how the biomass-derived oxygenates ethanol, isobutanol, 2,5-dimethylfuran (DMF), anisole, 4-methylanisole (4-MA), 2,4-xylene, and 2-phenylethanol (2-PE) impact fuel properties, as well as knock-limited spark advance and PM emissions from a single cylinder DISI engine.

**METHODS**

**Fuels and Fuel Property Measurements**

The base gasoline was obtained from a local supplier, and oxygenates were obtained as reagent grade chemicals. p-Xylene (1,4-dimethylbenzene) and p-cymene (1-methyl, 4-isopropylbenzene) were used to increase the base gasoline RON and PMI without adding oxygen. Blends were prepared volumetrically at room temperature, and the blend concentration was confirmed by an in-house gas chromatography method.

DHA was performed by ASTM method D6729. Our implementation of this method via gas chromatography has been previously reported [37]. Once the components were identified and quantified by gas chromatograph, an Excel spreadsheet containing each component name and the percent by weight present was generated. Because a few hundred components were present, we eliminated those present at less than 0.05 wt%, which resulted in less than a 5% total reduction in sample. Heat of vaporization (HoV) was calculated from the DHA as previously described [37].

The actual blend concentration of ethanol was determined by ASTM method D5501. Ethanol blends are designated by Exx, representing the nominal volumetric ethanol concentration. Other oxygenates were measured by an in-house two-dimensional heart-cutting gas chromatography method that has been previously described [26].

PMI was calculated from the DHA as in Aikawa et al. [13]

\[
PMI = \sum_{i=1}^{n} \left(\frac{[DBE_i+1]}{[PV(488K)]} \times W_t\right)
\]

(2)
where the double bond equivalent (DBE) of the individual compound is defined as:

\[ \text{DBE} = \frac{(2C + 2 - H)}{2} \]  

(3)

\( W_t \) is the weight percent of each component, and \( VP \) is the vapor pressure at 443K. Vapor pressures at 443 K were estimated following the Lee and Kesler method [38].

\[ P_{sat} = P_{sat}^0 \cdot P_c \]  

(4)

\[ \ln P_r^{sat} = (\ln P_r^{sat})^{00} + \omega (\ln P_r^{sat})^{11} \]  

(5)

\[ (\ln P_r^{sat})^{00} = 5.92714 - \frac{6.09648}{T_r} - 1.28862 \ln T_r + 0.169347 T_r^6 \]  

(6)

\[ (\ln P_r^{sat})^{11} = 15.2518 - \frac{15.6875}{T_r} - 13.4721 \ln T_r + 0.43577 T_r^6 \]  

(7)

where \( P_{sat} \) is the vapor pressure at a desired temperature, \( T_r \) is the reduced temperature (desired temperature/critical temperature), \( P_c \) is the critical pressure, and \( \omega \) is the acentric factor. Critical properties for individual compounds were taken from literature sources [39,40].

### Single-Cylinder Engine Experiments

The single-cylinder engine specifications are shown in Table 1. This engine was developed from a 2009 model year GM Ecotec 2.0 L LNF-series engine, with a wall-guided DI combustion system. The dynamometer, engine control, air handling, fuel supply, and combustion analysis systems have all been previously described [23]. A standard procedure for purging the fuel system and running the engine at a high power for a set period of time was performed before testing each new fuel.

Table 1. Single-cylinder engine specifications.

<table>
<thead>
<tr>
<th>Specification</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>Displacement (L)</td>
<td>0.5</td>
</tr>
<tr>
<td>Bore (mm)</td>
<td>86.0</td>
</tr>
<tr>
<td>Stroke (mm)</td>
<td>86.0</td>
</tr>
<tr>
<td>Connecting rod length (mm)</td>
<td>145.5</td>
</tr>
<tr>
<td>Compression ratio</td>
<td>9.2</td>
</tr>
<tr>
<td>Number of valves</td>
<td>4</td>
</tr>
<tr>
<td>Combustion System</td>
<td>Wall-guided Direct Injection</td>
</tr>
</tbody>
</table>

For spark timing sweep experiments, a relatively low engine speed was used because longer combustion duration increases exposure of the unburned end-gas to heat and pressure making the engine more sensitive to autoignition and knock. Experimental conditions were a nominal load of 925 kPa net mean effective pressure (NMEP), 1,500 rpm, and intake air temperature of 35°C (measured at the intake port). The load and intake air temperature were selected to ensure the engine could operate on the 88 RON hydrocarbon base gasoline. Cam phasing, fuel pressure, and start of injection were based on GM calibration data for this speed and load (see Table 2). Spark timing was initially set to 10 crank angle degrees (CAD) before top dead center (BTDC), fuel and air flows were adjusted slightly lean (0.3% - 0.5% oxygen in the exhaust gas). For each spark sweep the fuel and air flows were held constant after achieving the nominal 925 kPa NMEP load at 10° BTDC spark advance. Absolute fueling rates were unique to each blend because of energy and gravimetric density differences. Spark was then advanced in one or two degree increments. The engine output (load) increased up to minimum advance for best torque (MBT) because combustion phasing becomes optimal there.

Maximum pressure rise rate (MPRR) was used as a real-time measure of impending or actual knock, and spark timing was advanced until any cycle during the 100-cycle data collection period exceeded 1,100 kPa/CAD (the programmed limit triggering automatic spark retard). It should be noted that this MPRR limit turned out to be too aggressive (strong knock) and is not to be mistaken as a recommended practice. Integrated knock, or knock-integral (KI) was calculated by first filtering the in-cylinder pressure signal using a second-order Butterworth band-pass filter (5 - 15 kHz band), then rectifying the filtered signal [41]. A knock window was selected starting at 5° after top dead center and lasting for 30°. A reference window was selected starting at 210° BTDC and 30° duration. The filtered, rectified signal was then integrated separately over both the knock and reference windows. The KI value is defined by:

\[ KI = \frac{\int_{\text{Knock}}}{\int_{\text{Reference}} - \text{Threshold}} \]  

(8)

The threshold value chosen for this study was 0.5 KI units.

### Table 2. Engine operating parameters.

<table>
<thead>
<tr>
<th>Engine Speed/Load (rpm/kPa)</th>
<th>2,500/1,300</th>
<th>2,000/300</th>
<th>1,500/600</th>
<th>1,500/925 @ start of spark sweep</th>
</tr>
</thead>
<tbody>
<tr>
<td>Intake Press (bar abs)</td>
<td>1.15</td>
<td>0.46</td>
<td>0.70</td>
<td>0.86</td>
</tr>
<tr>
<td>Intake Temp (°C)</td>
<td>35</td>
<td>35</td>
<td>35</td>
<td>35</td>
</tr>
<tr>
<td>Fuel Rail Pressure (bar)</td>
<td>68</td>
<td>35</td>
<td>68</td>
<td>68</td>
</tr>
<tr>
<td>Start of Injection (°BTDC)</td>
<td>300</td>
<td>265</td>
<td>270</td>
<td>290</td>
</tr>
<tr>
<td>Spark Timing (°BTDC)</td>
<td>10</td>
<td>28</td>
<td>28</td>
<td>10, sweep starting point</td>
</tr>
<tr>
<td>Intake Cam Phasing (CAD)</td>
<td>30</td>
<td>30</td>
<td>35</td>
<td>40</td>
</tr>
<tr>
<td>Exhaust Cam Phasing (CAD)</td>
<td>20</td>
<td>25</td>
<td>30</td>
<td>35</td>
</tr>
<tr>
<td>Coolant / Oil Temp (°C)</td>
<td>85 / 90</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Equivalence Ratio</td>
<td>0.98</td>
<td></td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

*CAD advanced from full retard  **CAD retarded from full advance.*
Three separate engine speed and load operating points were used to evaluate fuel effects on PM-mass and PN emissions. These were 2,500 rpm-1,300 kPa NMEP; 2,000 rpm-300 kPa NMEP; and 1,500 rpm-600 kPa NMEP. Engine operating parameters for the PM experiments are shown in Table 2. The engine was operated slightly lean to ensure repeatable PM measurements, i.e., stoichiometric operation produced large PM measurement variations from minor air-fuel ratio instabilities. PM-mass, PN, and engine data were recorded for 1 minute at 1 Hz and then averaged. Each engine operating point was run several times in a randomized order across several days for each fuel.

The PN emission measurement system consists of a Dekati FPS-4000 two-stage exhaust sample dilution system upstream of a Dekati Thermodenuder feeding the diluted sample to a TSI Fast Mobility Particle Sizer (FMPS) model 3091. The Dekati dilution system uses a primary perforated wall flow type dilutor with dilution air that is temperature controlled (set to 150°C). The secondary stage of the dilutor is an ejector dilutor that uses room temperature dilution air and acts as the main driving force for the diluted exhaust sample flow. The overall dilution ratio was set to between 25:1 and 30:1 for all of the testing in this study. The Dekati Thermodenuder operating temperature was 275°C. The TSI FMPS measures PN distribution for particle diameters between 5.6 to 560 nm with a 32-channel resolution. The Thermodenuder is intended to remove all volatile compounds, so that the resulting FMPS measurements are theoretically on a strictly elemental carbon emissions basis. This sample processing was done because studies have shown that DISI engine vehicles equipped with a three-way exhaust catalyst emit primarily elemental carbon PM [22]. Separately, an AVL Micro-Soot Sensor (MSS) is connected to the raw engine exhaust and measures real-time PM-mass. The MSS includes contains its own built-in dilution system, which was nominally set to an 8:1 ratio.

RESULTS AND DISCUSSION

Fuel Properties

The properties of the gasoline base fuel have been reported previously [37], but are reproduced here for completeness. Compound classes and other properties of the base gasoline derived from the DHA are shown in Table 3. The base gasoline was a sub-octane blendstock for oxygenate blending intended for summertime use in an ozone non-attainment area. Particle emissions and PMI will be affected by aromatic and olefin content, and these values are in the middle range for U.S. gasoline [42].

Net heating values and boiling points for the oxygenates examined are shown in Figure 1, and other properties are listed in Table 4. The high boiling points of 2-PE and 2,4-xyleneol relative to the gasoline end point limit of 225°C are notable, as are the high volumetric energy densities of several of the oxygenates relative to conventional gasoline. All exhibit high octane number. The blending RON and MON values are reported in Table 4 because some of the compounds’ volatilities are too low to have their RON and MON measured directly. However, it must be noted that blending RON and blending MON cannot be considered absolute values because they depend on the chemistry of the base fuel and blending level. Furthermore, any errors in the octane numbers and concentration measurements are amplified by the equation for calculating these blending octane numbers, especially at low blending levels. For example, at the 20 vol% blend level, blending octane number can be computed as:

\[
\text{Blending Octane Number} = \frac{(\text{Blend ON}) - (0.8) \times (\text{Base Fuel ON})}{0.2}
\]

In this example, division by the volume fraction 0.2 results in a fivefold increase in error of the measured quantities in the resulting blending octane number.

| Table 3. PIANO analysis and other properties of the base gasoline. |
|-------------------------|-------------------|----------------|
| Paraffins               | D6729 vol%        | 11.5           |
| Isoparaffins            | D6729 vol%        | 47.9           |
| Aromatics               | D6729 vol%        | 23.7           |
| Naphthenes              | D6729 vol%        | 7.8            |
| Olefins                 | D6729 vol%        | 8.4            |
| Average MW              | D6729 g/mol       | 95.9           |
| Carbon                  | D6729 w%          | 86.1           |
| Hydrogen                | D6729 w%          | 13.9           |
| Density at 15°C         | D4052 g/ml        | 0.7374         |
| Dry vapor pressure equivalent (Reid vapor pressure equivalent) | D5191 Psi | 6.86 |
| Distillation T10        | D86 °C            | 61             |
| Distillation T50        | D86 °C            | 98             |
| Distillation T90        | D86 °C            | 154            |
| Final Boiling Point     | D86 °C            | 198            |

PIANO = paraffins, isoparaffins, aromatics, naphthenes, and olefins

Ethanol and isobutanol have high vapor pressure at 443 K and a DBE value of zero, so do not cause PMI to increase. DMF has a relatively high vapor pressure but a DBE of 3 and would be expected to moderately increase PMI. Anisole, 4-MA, 2,4-xyleneol, and 2-PE have much lower vapor pressures at 443 K and have DBEs of 4, causing PMI to increase. These expectations are met as shown in Table 5, which presents properties of the gasoline blendstock-oxygenate blends. Blends were also prepared with p-xylene (20 vol%) and p-cymene (20 vol%) to demonstrate the impacts of increasing aromatic content without fuel oxygen. The Sunoco GTX demonstrates that high aromatic content (45.5 vol%) can be offset by high vapor pressure at 443 K (note low T90) resulting in a low PMI fuel. Distillation curves of selected fuels are shown in Figure 2. Blending with 20 vol% 2-PE causes the gasoline to fail the maximum limit for T90 and nearly fail for T50. The 10 vol% 2,4-xyleneol blend nearly fails T90 and the 21% 4-MA blend nearly fails T50. The relatively high boiling point of these oxygenates significantly limits levels that can be blended into ASTM D4814-compliant gasoline.
Figure 1. Boiling point and net heating value for the biomass-derived oxygenates.

Figure 2. Distillation curves by ASTM method D86 for gasoline oxygenate blends. Limits shown are for Class AA or Class A volatility class gasoline.

Table 4. Properties of biomass-derived oxygenates.

<table>
<thead>
<tr>
<th>Compound</th>
<th>Structure</th>
<th>Blending RON / MON&lt;sup&gt;b&lt;/sup&gt;</th>
<th>HoV (kJ/kg)&lt;sup&gt;13&lt;/sup&gt;</th>
<th>Net Heating Value (MJ/L)</th>
<th>Vapor Pressure @ 443 K (kPa)</th>
<th>Boiling Point (°C)&lt;sup&gt;8,46&lt;/sup&gt;</th>
<th>DBE</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ethanol</td>
<td></td>
<td>131 / 103&lt;sup&gt;b&lt;/sup&gt;</td>
<td>921</td>
<td>21.4&lt;sup&gt;44&lt;/sup&gt;</td>
<td>1,550</td>
<td>78</td>
<td>0</td>
</tr>
<tr>
<td>Isobutanol</td>
<td></td>
<td>116 / 88</td>
<td>634</td>
<td>26.6&lt;sup&gt;44&lt;/sup&gt;</td>
<td>596</td>
<td>108</td>
<td>0</td>
</tr>
<tr>
<td>2,5-Dimethylfuran (DMF)</td>
<td></td>
<td>141 / 104</td>
<td>379</td>
<td>30.1&lt;sup&gt;44&lt;/sup&gt;</td>
<td>538</td>
<td>94</td>
<td>3</td>
</tr>
<tr>
<td>Anisole</td>
<td></td>
<td>124 / 102</td>
<td>419</td>
<td>33.2&lt;sup&gt;4&lt;/sup&gt;</td>
<td>154</td>
<td>154</td>
<td>4</td>
</tr>
<tr>
<td>4-Methylanisole (4-MA)</td>
<td></td>
<td>129 / 99</td>
<td>377</td>
<td>33.4&lt;sup&gt;4&lt;/sup&gt;</td>
<td>87.7</td>
<td>174</td>
<td>4</td>
</tr>
<tr>
<td>2,4-Xylenol</td>
<td></td>
<td>197 / 159</td>
<td>530</td>
<td>34.2&lt;sup&gt;4&lt;/sup&gt;</td>
<td>30.3</td>
<td>211</td>
<td>4</td>
</tr>
<tr>
<td>2-Phenylethanol (2-PE)</td>
<td></td>
<td>132 / 99</td>
<td>561</td>
<td>34.8&lt;sup&gt;4&lt;/sup&gt;</td>
<td>21.5</td>
<td>220</td>
<td>4</td>
</tr>
<tr>
<td>p-Xylene</td>
<td></td>
<td>124 / 97</td>
<td>399</td>
<td>35.4&lt;sup&gt;45&lt;/sup&gt;</td>
<td>218</td>
<td>138</td>
<td>4</td>
</tr>
<tr>
<td>p-Cymene</td>
<td></td>
<td>124 / 101</td>
<td>365</td>
<td>35.5&lt;sup&gt;45&lt;/sup&gt;</td>
<td>84.5</td>
<td>177</td>
<td>4</td>
</tr>
</tbody>
</table>

<sup>*For blends in this work. ¹For E25. ²This work.*
Table 5. Properties of the gasoline blendstock, its oxygenate blends and control fuels.

<table>
<thead>
<tr>
<th>Fuel Blend</th>
<th>Blend Level (wt% / vol%)</th>
<th>Oxygen (wt%)</th>
<th>RON / MON</th>
<th>ηHv at 25°C (kJ/kg)</th>
<th>Net Heating Value (MJ/L)</th>
<th>T_{90}/T_{95} °C</th>
<th>PMI</th>
</tr>
</thead>
<tbody>
<tr>
<td>Base Fuel</td>
<td>--</td>
<td>0</td>
<td>87.9 / 81.9</td>
<td>352.8</td>
<td>32.1</td>
<td>98 / 154</td>
<td>1.07</td>
</tr>
<tr>
<td>Ethanol (E10)</td>
<td>9.9 / 9.3</td>
<td>3.5</td>
<td>93.0 / 84.1</td>
<td>415.5</td>
<td>30.8</td>
<td>86 / 152</td>
<td>0.97</td>
</tr>
<tr>
<td>Ethanol (E25)</td>
<td>27.6 / 26.0</td>
<td>9.6</td>
<td>99.1 / 87.4</td>
<td>527.3</td>
<td>29.1</td>
<td>72 / 146</td>
<td>0.80</td>
</tr>
<tr>
<td>Ethanol (E50)</td>
<td>49.2 / 47.1</td>
<td>17.1</td>
<td>102.6 / 88.7</td>
<td>662.3</td>
<td>26.8</td>
<td>75 / 81</td>
<td>0.58</td>
</tr>
<tr>
<td>Isobutanol</td>
<td>16.7 / 15.5</td>
<td>3.6</td>
<td>92.3 / 82.8</td>
<td>398.4</td>
<td>31.0</td>
<td>93 / 149</td>
<td>0.92</td>
</tr>
<tr>
<td>2,5-Dimethylfuran (DMF)</td>
<td>20.1 / 17.0</td>
<td>3.4</td>
<td>96.9 / 85.6</td>
<td>371.4</td>
<td>31.6</td>
<td>96 / 147</td>
<td>1.01</td>
</tr>
<tr>
<td>Anisole</td>
<td>24.7 / 19.6</td>
<td>3.7</td>
<td>95.0 / 85.8</td>
<td>371.8</td>
<td>32.3</td>
<td>115 / 154</td>
<td>1.61</td>
</tr>
<tr>
<td>4-Methylanisole (4-MA)</td>
<td>26.3 / 21.4</td>
<td>3.5</td>
<td>96.7 / 86.5</td>
<td>360.6</td>
<td>32.4</td>
<td>122 / 173</td>
<td>2.20</td>
</tr>
<tr>
<td>2,4-Xylenol</td>
<td>13.3 / 10.0</td>
<td>1.8</td>
<td>98.8 / 89.6</td>
<td>371.1</td>
<td>32.3</td>
<td>103 / 189</td>
<td>3.13</td>
</tr>
<tr>
<td>2-Phenylethanol (2-PE)</td>
<td>22.3 / 17.2</td>
<td>2.9</td>
<td>95.4 / 86.0</td>
<td>399.5</td>
<td>32.5</td>
<td>112 / 212</td>
<td>6.03</td>
</tr>
<tr>
<td>p-Xylene</td>
<td>25.5 / 20.0</td>
<td>0</td>
<td>95.1 / 84.9</td>
<td>363.2</td>
<td>32.6</td>
<td>112 / 146</td>
<td>1.36</td>
</tr>
<tr>
<td>p-Cymene</td>
<td>23.3 / 20.0</td>
<td>0</td>
<td>95.3 / 85.7</td>
<td>347.8</td>
<td>32.7</td>
<td>118 / 173</td>
<td>2.19</td>
</tr>
<tr>
<td>Sunoco GTX</td>
<td>--</td>
<td>0</td>
<td>103 / 93</td>
<td>364.2</td>
<td>32.6</td>
<td>104 / 108</td>
<td>0.70</td>
</tr>
</tbody>
</table>

**Single-Cylinder Engine Results**

**Knock Limited Spark Advance**

KI averages of 100 engine cycles versus spark advance for all fuels tested are shown in Figure 3. Inspection of the cylinder pressure curves for knock, led to selecting the knock-limited spark advance (KLSA) level as occurring at KI = 10. This was correlated with MPRR values of 500 ±30 kPa/CAD, and above this level the engine was experiencing knock. Among the non-oxygenated control fuels, the 87.9 RON base fuel exhibited a KLSA of 14° BTDC, the p-xylene blend (RON 95.1) had a KLSA of 19° BTDC, the p-cymene (RON 95.3) blend had a KLSA of 19.5° BTDC, while the 103 RON Sunoco GTX was far removed from knock at this operating condition. It is worth noting that some fuels exhibited different slopes as KI rapidly increased, and in particular the slope for the E25 blend was lower, and remained lower crossing the KLSA level than did slopes for the other fuels.

Figure 4 plots KLSA versus RON for all fuels studied except for E50 and Sunoco GTX, which were not knock limited in this engine at the test conditions. In the octane index proposed by Kalghatgi (Equation 1), RON is the case where K = 0 and linear regression produced a correlation coefficient, R^2 = 0.870. Table 6 summarizes correlation coefficients for KLSA against a series of OIs with K ranging from 1 to -0.25. The maximum correlation was when K = 0.25. From this analysis it appears that K for this engine and operating condition approximates the RON method. This is reasonable given the low intake air pressure and temperature, spark timing near minimum advance for best torque (MBT), and modest compression ratio [6,47].

Spark sweep results for the control fuels and non-ethanol oxygenate blends that had distillation T_{90} less than or equal to that for the base fuel are shown in Figure 5. The low octane base gasoline exhibited a KLSA of 14° BTDC, and triplicate spark sweeps revealed a maximum NMEP standard deviation of 3.6 kPa at 12° BTDC, while the average standard deviation was less than 2 kPa. The MBT spark advance for DMF and anisole blends was 20° BTDC, as indicated by the peak NMEP. The p-xylene blend had strong knock (at the maximum pressure rise rate limit) at 20° BTDC in spite of having 95.1 RON, similar to the anisole blend.
more of the fuel to evaporate than in a DISI engine. These differences may explain the observed variance between 2-PE’s KLSA measured in the DISI engine and the measured RON.

In addition to fuel autoignition chemistry, knock resistance for DISI engines may be enhanced by fuel-air charge cooling as the fuel evaporates, which reduces the end-gas temperature. This is an important effect in DISI engines regardless of fuel type. The HoV of gasoline hydrocarbons is 350 to 400 kJ/kg at 25°C while that of ethanol is 920 kJ/kg [37,48]. As shown in Table 4, several of the biomass-derived oxygenates also exhibit HoV significantly higher than that of gasoline boiling range hydrocarbons and thus potentially have knock resistance over and above that provided by their high RON. However, as shown in Table 5, in most cases the impact on HoV is relatively small, the exceptions being the E25 and E50 blends. Based on their similar RONs of ~99, it would be expected that the 2,4-xylene and E25 blends would have the same KLSAs. However, as Figure 7 shows, E25 was able to tolerate additional spark advance (24.3° BTDC) compared to the 2,4-xylene blend (22° BTDC) before reaching KLSA. The HoV for the E25 blend was calculated to be 527 kJ/kg and that for the 2,4-xylene blend was 371 kJ/kg (see Table 5), the latter being close to the base gasoline’s. Thus, additional charge cooling from ethanol in
the E25 blend may explain the enhanced KLSA performance of this fuel. Another factor may have been reduced knock resistance from 2,4-xylenol for the same reasons postulated for 2-PE, given the similarly high boiling point of this molecule.

Because we are reporting the number of particles that fall within each bin, the result would appear that there are 80 times more particles in the largest bin than in the smallest bin because it is 80 times wider. To overcome this problem, the particle number is normalized by the width of its respective bin. The particle count is roughly divided by 1 for the smallest bin and 80 for the largest bin so that it shows a more representative distribution of particle count across the size range for each channel.

**Particle Emissions**

Figure 8 shows the PM-mass results for all three speed-load conditions. The E10 fuel data were anomalous and discarded from the particle emission results because of suspected fuel cross-contamination from the engine lube oil. At the lowest load condition (bottom panel), PM-mass concentrations are very low and it is difficult to discern differences between fuels. PM-mass emission levels at this condition may be below or only slightly above the detection limit of our measurement system for most fuels. Nevertheless, the PM-mass emissions from the p-xylene control fuel and 4-MA were clearly higher than from the base gasoline, as expected from their higher PMIs. More differentiation is apparent at the intermediate load (center panel), but at 2,500 rpm-1,300 kPa NMEP PM-mass emissions are 2 to 10 times higher. Here, fuel effects are evident with significantly higher (statistical p-value < 0.01) emissions observed for fuels spiked with aromatic/low vapor pressure components (components with high PMI) relative to the base gasoline. The fuel effects on engine exhaust total PN concentration can be seen in Figure 9 for the 2,500 rpm-1,300 kPa NMEP condition. The error bars represent the 95% confidence interval. As was the case for the PM-mass results, PN emissions showed much higher emission levels than from the lower load points, and generally revealed the expected trends of higher emissions (p < 0.01) with higher PMI fuels relative to the base gasoline.

Particle size distribution plots are displayed on a log-log chart. The x-axis of particle diameter is fairly straightforward but the y-axis of PN dN/dlogDp is not. The FMPS measures particles in the size ranges from 5.6 to 560 nm. This range is split into 32 channels or bins. The smallest diameter size bin counts particles with a nominal or midpoint size of 6.04 nm and the bin boundaries are roughly 0.5 nm above and below that. The largest diameter size bin counts particles with a nominal midpoint diameter of 523.3 nm and the bin ranges roughly 40 nm above and below that. The bin for the largest diameter particles is roughly 80 times wider than the smallest bin.

Examination of the data in Figure 10 for operation at 2,500 rpm-1,300 kPa shows very similar size distribution for all fuels with a nucleation mode centered at about 10 nm and accumulation mode centered at 60 to 70 nm. The data are generally consistent with the total PN results; for example, the E50 blend showed the lowest PM-mass and total PN emissions, consistent with the much lower level of particles in the accumulation mode. The correlation between particle number and particle mass concentrations at 2,500 rpm-1,300
kPa is shown in Figure 11. The strong correlation is expected for particles that are predominantly elemental carbon, accumulation-mode particles [22,23].

Isobutanol and DMF slightly increased PM-mass and PN over the base gasoline at 2,500 rpm-1,300 kPa despite having slightly lower PMIs (0.92 and 1.0, respectively), which may simply reflect small measurement errors in both PM emissions and in the parameters used to estimate PMI. However, higher isobutylene emissions have been measured from an isobutanol-gasoline fueled vehicle, so it is possible that in-cylinder isobutylene formation contributed to molecular weight growth and therefore to PM [49]. In the case of DMF, once the furan ring opens, reactive olefins are likely produced, which similarly may lead to molecular weight growth.

Figure 12 shows the correlation between PM-mass concentration and PMI, while Figure 13 shows the correlation between PN concentration and PMI. For most fuels there was good correspondence of PM-mass and PN emissions with PMI; however, in both cases results for 2,4-xyleneol and 2-PE were not included in the linear regression as they fall significantly away from the trend for the other fuels, emitting less PM than predicted by PMI. The lowest PM-mass and PN emissions were observed for E50, which also had the lowest PMI (0.58) and the highest fuel oxygen content. E25 and Sunoco GTX each have PMIs between those for the base gasoline and E50, and their PM-mass emissions fall in between, as expected.
The difference in results between 4-MA and p-cymene, which have the same PMIs, was also unexpected because they have nearly identical boiling points and vapor pressures (at 443 K), and produced similar knock-limited performance (see Figure 6). Yet 4-MA produced higher PM-mass and PN emissions. Studies of anisole pyrolysis show that its decomposition proceeds through homolysis of the O-CH₃ bond to phenoxy radical. This further decomposes to cyclopentadienyl radical, which can couple to form naphthalene initiating chain or molecular weight growth [50,51]. No similarly facile route to phenoxy radical exists for aromatic hydrocarbons, which must add oxygen to the ring. Taken as a whole, these observations for isobutanol, DMF, and 4-MA suggest that combustion effects may exist for blending some oxygenates with gasoline that are not captured by the current PMI relationship (Equation 2).

In comparing results for both PM-mass and PN to the PMI predicted trend, both 2-PE (PMI = 6.0) and 2,4-xylene (PMI = 3.1) are not as high as expected. It is notable that both of these blend components boil above 200°C, significantly increase the blend T₉₀, and have the lowest vapor pressures at 443 K of all of the oxygenates tested. The T₉₀ for the 2-PE blend is well above the allowable T₉₀ limit for gasoline in ASTM D4814. As discussed above, 2-PE underperformed for knock resistance; we speculated that this was caused by 2-PE failing to fully evaporate, therefore being depleted in the end gas. Incomplete evaporation may also be the reason for the lower than expected PM-mass and PN emissions from 2-PE and 2,4-xylene. The T₉₀ limit for gasoline exists, in part, to protect engines from accumulation of unburned fuel in the lubricant. While it is anecdotal, we observed by smell that the engine lube oil retained the four lowest vapor pressure fuels, each of which has a distinctive odor, supporting the idea that these blend components do not fully evaporate. This idea further is supported by data in Figure 14 that show a strong correlation between total hydrocarbon emissions and PM-mass. If 2-PE and 2,4-xylene were evaporating but not combusting (therefore also not forming PM), we would expect anomalously high total hydrocarbon (THC) emissions relative to the other fuels. But this was not the case.

The difficulty in fully evaporating the high boiling 2-PE and 2,4-xylene may have been enhanced by engine operating parameters. At 2,500 rpm-1,300 kPa NMEP, the start of injection was 300° BTDC (i.e., 60° after the start of the intake stroke), so the piston was still relatively high in the cylinder and accelerating down while the injector pulse widths were the longest (~3.5 mS) of all test points. Consequently, fuel spray impingement on the piston and/or cylinder wall was possible. This combined with low volatility and low reactivity fuel components may have made their evaporation and combustion difficult.

CONCLUSIONS

Our objective in this work was to determine the effects of a small group of oxygenated molecules, representative of those that could be derived from biomass, on DISI engine knock-resistance and particle emissions. The high octane oxygenates were blended with a sub-octane gasoline blendstock intended for blending with ethanol. Fuel properties of the blends were measured, and a modern DISI engine was used to measure their knock resistance and PM emissions. Two of the oxygenates, 2-PE and 2,4-xylene, significantly increased the T₉₀ distillation temperature in the D86 distillation curve. The 20% 2-PE blend failed the T₉₀ limit for gasoline. The high boiling points of these oxygenates will significantly limit their use in gasoline, probably to less than a few vol%.

It was found that RON was a good predictor of knock-limited performance for all fuels tested, consistent with an estimated K value of 0 to 0.25 for the engine operating conditions used in the study. The 2-PE blend underperformed in terms of a lower KLSA than the blended p-xylene and p-cymene control fuels, which had the same RON. We speculate that 2-PE’s lower KLSA was associated with its low volatility leading to depletion of 2-PE in the end gas. The E25 blend was found to have a higher KLSA than the 2,4-xylene blend with the same RON, possibly because of ethanol’s enhanced charge cooling in the DISI engine. An additional factor may have been reduced knock resistance of 2,4-xylene for the same reasons postulated for 2-PE, given the similarly high boiling point of this molecule.

Particle emission effects of the fuels were revealed at the highest load condition employed of 2,500 rpm and 1,300 kPa NMEP. Isobutanol produced a small increase in both PM-mass and PN emissions, similar to that from DMF. This was inconsistent with isobutanol’s relatively low boiling point, high vapor pressure, and lack of unsaturated structures. Anisole, 4-MA, 2-PE, and 2,4-xylene caused a significant increase in both PM-mass and PN emissions (by factors ranging from 2 to 5) relative to the base gasoline. Thus, any effect of their oxygen atom to reduce PM by increasing local air-fuel ratio is outweighed by their low vapor pressure and high DBE values. The boiling point of 2-PE (220°C) and 2,4-xylene (211°C) and their very low vapor pressures may have significantly altered performance properties that are critical to DISI engine performance. Yet PM-mass and PN emissions were lower than would be predicted by correlation with PMI, suggesting abnormal or incomplete combustion. Consistent with the knock resistance results, these high boiling blend components likely did not fully evaporate and were swept into the lube oil, making them unavailable for particle formation.
Results for several of the oxygenates suggest that the current equation for calculating PMI does not include factors capturing all chemical effects of oxygenates blended into gasoline on PM emissions. Additional investigation of this is warranted.

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DEFINITIONS/ABBREVIATIONS
2-PE - 2-phenylethanol
4-MA - 4-methylanisole
BTDC - before top dead center
CAD - crank angle degree
DBE - double bond equivalent
DHA - detailed hydrocarbon analysis
DI - direct injection
DISI - direct injection spark ignition
DMF - 2,5-dimethylfuran
Exx - percent ethanol
FMPS - fast mobility particle sizer
HoV - heat of vaporization
KI - integrated knock, or knock-integral
KLSA - knock limited spark advance
MBT - minimum advance for best torque
MON - motor octane number
NMEP - net mean effective pressure
OI - octane index
PM - particulate matter
PMI - particulate matter index
PN - particle number
RON - research octane number
rpm - revolutions per minute
S - octave sensitivity (RON - MON)
SI - spark ignition
T50 - temperature at 50% distilled
T90 - temperature at 90% distilled
THC - total hydrocarbons
wt% - percent by weight