Use Steam Jet Ejectors or Thermocompressors to Reduce Venting of Low-Pressure Steam

Large industrial plants often vent significant quantities of low-pressure steam to the atmosphere, wasting energy, water, and water-treatment chemicals. Recovery of the latent heat content of low-pressure steam reduces boiler load, resulting in energy and fuel cost savings. Low-pressure steam's potential uses include driving evaporation and distillation processes, producing hot water, space heating, producing a vacuum, or chilling water. If the steam pressure is too low for the intended application, a steam jet thermocompressor can boost the pressure and temperature to the required level.

Operating Principles
Thermocompressors and ejectors operate on the same thermodynamic and physical principle: energy contained in high-pressure steam can be transferred to a lower pressure vapor or gas to produce a mixed discharge stream of intermediate pressure. These devices are known for:

- Simple construction
- Insensitivity to fouling
- Easy installation
- Low capital and installation costs
- Easy maintenance with no moving parts
- Long useful operating lives

If the objective is to recover the latent heat content of the low-pressure suction vapor for process use, the device is called a thermocompressor. If the objective is to pull a vacuum on a process vessel, the device is called an ejector.

Boosting Steam Pressure and Temperature with Thermocompressors
Single or multi-stage thermocompressors are used to boost low-pressure vent steam to a useful higher pressure and temperature. When high-pressure motive steam is available, thermocompressors can be economically used for compression ratios up to 6:1 (absolute pressure of supply steam/suction steam).

Figure 1. Typical Thermocompressor Application
High-pressure motive steam supplied to the thermocompressor expands in a converging-diverging nozzle to convert pressure energy to kinetic energy. Vent steam supplied to the suction port is entrained into this low-pressure/high-velocity jet, where mixing occurs. The diffuser portion of the thermocompressor (Figure 1) reconverts the kinetic energy of the mixture back into pressure. The intermediate discharge pressure is between the pressure of the motive and low-pressure suction steam. Discharge pressure is determined by the compression ratio (i.e., the ratio of the pounds per hour [lbs/hr] of motive steam supplied to the lbs/hr of low-pressure suction steam entrained). Thermocompressor capacity of the device is dictated by the availability of motive steam, motive and suction steam pressure, and discharge steam pressure requirements. Applications include drying and heating, multi-effect evaporators, vulcanizers, reboilers, strippers, condensate receiver tanks, and solvent extraction processes.

Producing a Vacuum with Steam Jet Ejectors

In a vacuum jet ejector, the low-pressure vent steam is the motive energy source. Air and/or water vapor are sucked from the process into the mixing chamber at near-vacuum conditions. Both the motive vent steam and the suction vapors/gases pass through a venturi throat and are released through a diffuser. Although steam jet ejectors can be used to pull a vacuum with motive steam pressure as low as 5 pounds per square inch gauge (psig), higher pressures of 15 to 50 psig are more practical.

Example

An industrial facility vents 10,000 lbs/hr of steam at near atmospheric pressure (0.3 psig, 212.9°F); 1,150.7 British thermal units per pound (Btu/lb) can convert wasted steam into useful low-pressure process steam by boosting its pressure to 15.3 psig (250.3°F, 1,164.1 Btu/lb). Saturated motive steam at a pressure of 200 psig is available (387°F, 1,199.7 Btu/lb).

For a required compression ratio of 2:1 (15.3 + 14.7 psia) / (0.3 + 14.7 psia), 1.1 pound of high-pressure motive steam per pound of low-pressure suction steam is required. The thermocompressor requires 11,000 lbs/hr of 200 psig steam to produce a discharge of 21,000 lbs/hr of 15.3 psig intermediate pressure steam. Elimination of steam venting saves:

**Energy Savings = Vent steam flow rate (lbs/hr) x Enthalpy of the vented steam less the enthalpy of makeup water (Btu/lb)**

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\text{Energy Savings} = 10,000 \text{ lbs/hour} \times (1,150.7 - 77) \text{ Btu/lb} = 10.7 \text{ MMBtu/hr}
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For a continuously operating facility, annual energy savings are approximately 94,000 MMBtu per year. For natural gas fuel priced at $5.00 per MMBtu with a boiler efficiency of 80%, fuel savings are valued at:

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94,000 \text{ MMBtu/yr} \times \frac{$5.00}{\text{MMBtu}} \times 0.80 = $587,500/\text{yr}
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