



Photo from iStock 547150468

# Anaerobic Digestion of Food Waste: Products and Their Uses

## Introduction

Anaerobic digestion (AD) is a relatively simple biologically mediated, thermodynamically driven carbon management process carried out in the absence of oxygen. A self-establishing consortium of bacteria comprising hydrolyzers, acidogens, acetogens, and methanogens convert complex organic compounds into simpler molecules (hydrolyzers), simple molecules into volatile fatty acids (VFAs) (acidogens), VFAs into acetic acid (acetogens), and acetic acid into biogas (methanogens) to derive energy and metabolic building blocks. In contrast to aerobic digestion, which converts organic waste primarily to microbial biomass and carbon dioxide (CO<sub>2</sub>), AD generates mainly methane and digestate. Typically, AD is used to treat large volumes of diverse, high-strength organic waste, as it is less capital intensive, has lower operating costs, and takes up less space than a comparable aerobic system.

At steady state, the outputs from traditional AD units are biogas and digestate. The biogas is primarily made up of methane (CH<sub>4</sub>) and CO<sub>2</sub>, with traces of hydrogen (H<sub>2</sub>) and/or hydrogen sulfide (H<sub>2</sub>S). These gases leaving the system “pull” the remaining complex molecule conversions through the consortial metabolism of converting complex organic compounds to biogas. If the methanogens that convert the acetate to biogas are inhibited, the acetate and VFAs build up and “sour” the digester by stopping the consortium from functioning. This is a primary concern for AD of food waste, as methanogens are particularly sensitive to low pH, which can be caused if high VFA production rates from acidogens and acetogens (using easy-to-digest compounds found in food waste) exceed the

methanogenesis rate. Food waste often has high protein levels as well, and ammonia production during proteolysis can also inhibit the methanogens. The key to a functional digester is keeping the methanogens happy.

The feed rate into the system is equal to the output rate of biogas plus the digestate (solids plus liquor or “centrate”). The solids are composed of undigested feed material and the microbial biomass produced. The liquor contains water plus any soluble organic compounds and salts. When the digestate results from anaerobic digestion of sewage, the solids are referred to as biosolids. The fraction of input solids converted is typically between 40%–60% and is dependent on many factors such as solids retention time, feedstock composition, digester configuration, and digester operating conditions. Many AD operations use chemical oxygen demand as a metric to determine the extent of digestion. Although chemical oxygen demand is simple and easy to measure, it was originally developed as a measure of water quality and tells you nothing about the composition of the organic compounds in the sample. This may be enough for the purposes of the U.S.

**Note: Research into anaerobic digestion of food waste, especially on uses for digestate, is limited in comparison to sewage and manure. However, there is little reason that technologies developed for these large-volume feedstocks cannot be applied to food waste digestate in many cases. This summary includes sewage-based biosolids conversion methods where they could be applicable to food waste digestate.**

Environmental Protection Agency, but it provides no detailed information about which components are converted or which remain in the digestate. Because the value of the digestate is often determined by its composition, more detailed chemical analyses are required. However, there is no current standard by which this can be measured, as discussed in the following sections.

## Biogas

The major market product from anaerobic digestion is biogas, specifically the CH<sub>4</sub> fraction. Typically, CH<sub>4</sub> makes up about 60% of the biogas, ±10%, with CO<sub>2</sub> comprising most of the remainder. The key use of CH<sub>4</sub> is as an energy source to produce heat, electricity, and renewable natural gas that could be injected into the pipeline system or used as a transportation fuel. As such, it needs to be cleaned up and upgraded in most cases. CO<sub>2</sub> needs to be removed to increase the thermal value and decrease emissions. This is often done by water stripping or pressure swing adsorption. H<sub>2</sub>O, H<sub>2</sub>, H<sub>2</sub>S, and some nitrogen compounds are usually found at low levels in biogas. H<sub>2</sub>O lowers the heating value and causes corrosion issues. H<sub>2</sub>S is toxic and corrosive and must be mitigated in most cases, usually by adding in air/O<sub>2</sub> to oxidize it or reacting with an iron compound to convert it to less-toxic iron sulfide and H<sub>2</sub>. Another consideration is that increasing the amount of biogas produced not only increases the methane, but it also reduces the amount of biosolids. Basically, every kilogram of biogas made is one less kilogram of biosolids that requires disposal or other use.

Increasing the CH<sub>4</sub> fraction of biogas can improve the economics by providing more product and reducing cleanup costs. Thermophilic AD has been shown to increase CH<sub>4</sub> production.<sup>1</sup> Balancing feedstock inputs using co-digestion strategies can increase CH<sub>4</sub> production, as can developing



Photo from iStock 499190705

better consortia.<sup>2-7</sup> Feedstock pretreatment can also be used to increase both CH<sub>4</sub> production and feedstock utilization. Thermal, chemical, thermochemical, mechanical processing, enzyme, and other preprocessing of the feedstock has been shown to increase CH<sub>4</sub> production and the rate and extent of conversion of multiple feedstocks.<sup>1, 8-14</sup>

What to do with the CO<sub>2</sub> is another consideration. Around 30%–40% of the biogas is typically CO<sub>2</sub>. It is low value and limited in use—for example, it cannot be used in food processing. Certain microbes can convert it to methane if given enough H<sub>2</sub>. Recent advances in this area made by the National Renewable Energy Laboratory have demonstrated the efficient conversion of biogas CO<sub>2</sub> to methane using a pressurized microbial bioreactor fed with biogas and H<sub>2</sub> produced by electrolysis of water.<sup>15</sup> Using renewable electricity to produce the H<sub>2</sub> makes this process 100% renewable, and it can be bolted on to any biogas system. Alternatively, the CO<sub>2</sub> could be a good candidate for carbon sequestration, as this CO<sub>2</sub> is organically derived and is a concentrated point source of carbon. It has even been suggested that the CO<sub>2</sub> could be used to grow algae to facilitate nutrient removal from AD centrate and generate bioproducts from the algae.<sup>16</sup>

## Digestate

Anaerobic digestate is the combined liquid and solid fractions left after the AD process. The solids fraction comprises undigested feedstock and microbial biomass produced as a result of growth in the digester. Typically, the inorganic content is the same as the feedstock (i.e., same potassium, phosphorous, and nitrogen levels), as most of the mass loss is from organic (i.e., carbon) degradation. The chemical composition varies, primarily as a function of the feedstock and digestion parameters, but it often contains high fractions of cellulose, lignin, and some protein. Due to the retained nutrient value, it is most often used as a fertilizer, though application is restricted in certain areas. Additional pressures limiting landfiling of organics in many areas are also driving the need for additional outlets for digestate. Due to the large volume of sewage treatment, there has been a great amount of research on conversion of biosolids to products. Similar efforts in food waste digestate have lagged but are increasing with the recent emphasis on diversion away from landfills and limits on land application due to nutrient and heavy metal buildup in soils. The current options for food waste digestate are diagrammed in Figure 1 and detailed in the following sections.

### Solid-Liquid Separation

The solid-liquid ratio of AD feed streams is highly dependent on the source and has a large impact on the digester design, operation, and handling costs. In general, AD can be characterized as “wet” (<10% total solids), “semi-dry” (10%–15% total solids), or “dry” (>15% total solids).<sup>17</sup> Higher total solids can be handled in smaller digesters with lower capital costs, and low moisture content in the digestate means lower volume to

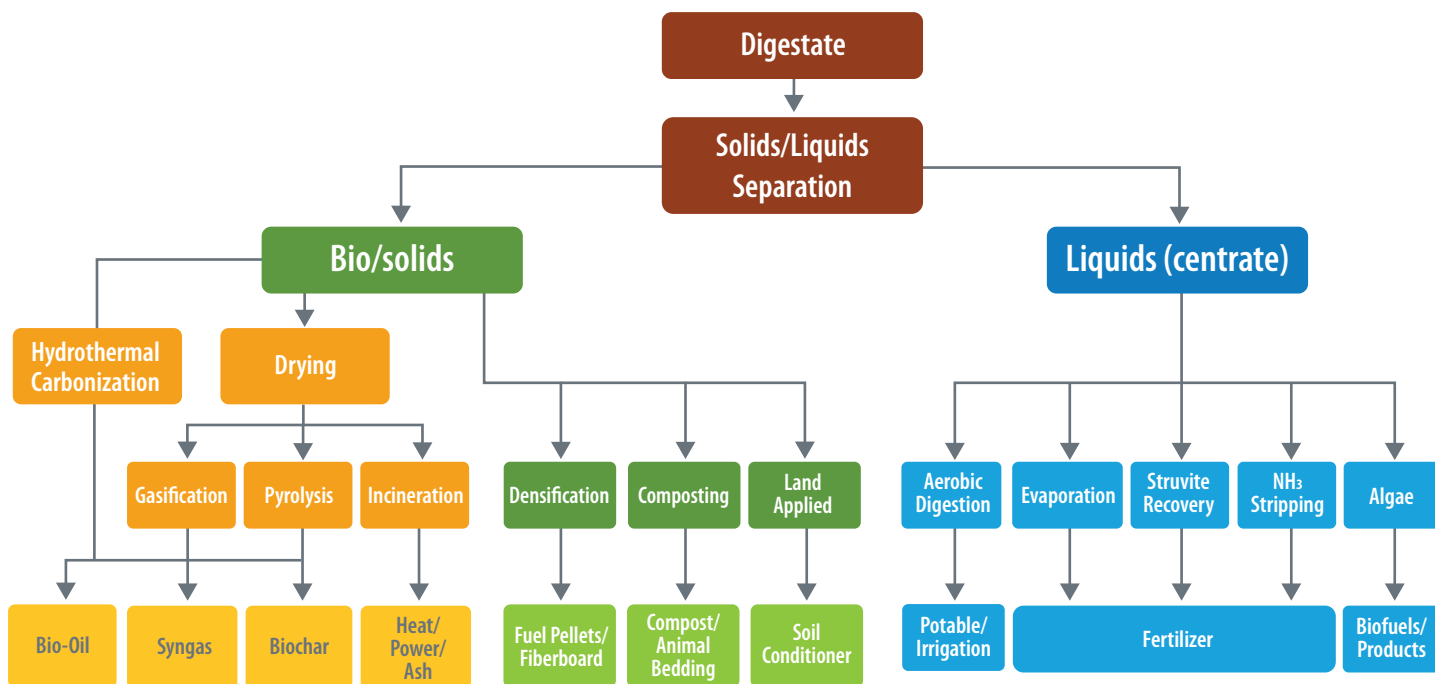


Figure 1. Current and potential uses for food waste digestate

transport and process. On the other hand, mixing is easier with higher water content, and pumps can be used to move the components around. Higher water content also provides for lower concentrations of VFAs and ammonium compared to high solids, providing better conditions for methanogens.

Adjusting the solid-liquid ratio often requires a solid-liquid separation—or dewatering—step. This dewatering, or thickening as it is often called, is a major unit operation at many AD plants, and numerous companies and methods are available to facilitate this effort. Settling, microbial or chemical flocculation and/or coagulation, centrifugation, chemo- or electro-oxidation, acidification, air drying, hydrothermal treatment, ultrasound, electrochemical precipitation, pressing, and filtration have all been studied or employed in AD solid-liquid separation.<sup>18-30</sup> Recent studies using biochar as an AD additive have demonstrated positive benefits in both methane production and dewatering parameters, though the impact of the biochar on the digestate end use should be considered.

## Land Application

The most common use for digestate is land application. It typically has high fertilizer value, and the organic content is useful in restoring lands where topsoil has been removed, such as mining sites and deforested lands. Smaller-scale applications include compost, home and garden fertilizer, landscaping mulch, and even as eco-friendly decomposable planters. For example, Bloom is a commercial mulch derived from a water treatment plant in Washington, D.C.<sup>31</sup> It is available in bulk for commercial and agricultural use, dried and packaged for home and small business, and blended with woody biomass or sand for specific applications.

Digestate solids from food waste are processed similarly. The primary limitation to land application is transportation cost. Digestate is expensive to transport and apply, so land application is typically carried out close to the site of production. As a result, the land immediately surrounding an AD plant rapidly becomes saturated with nutrients, and regulatory limits restrict further application. Eventually, longer distances preclude economic transport and other uses of the digestate need to be developed.

Depending on the soluble compounds present, the centrate can be processed to generate fertilizer (from high phosphorus and nitrogen containing systems). The concentration and processing has been demonstrated to consume approximately 10% of the total energy produced by the digester<sup>32</sup> using evaporation and reverse osmosis processing. This can be combined with specific nutrient removal via ammonia stripping and struvite precipitation to generate nitrogen-balanced fertilizers. Because phosphorus is a major component in many AD centrate streams, there is high interest in recovering this diminishing resource for multiple reasons. Removing phosphorus can mitigate operational issues with struvite formation in pipes and tankage. Also, because many digestate-treated lands are becoming overloaded with phosphorus, removing it could allow continued application in nearby lands. Lastly, concentrated phosphorus can be used in fertilizer and transported to distant areas that are phosphorus-deplete.

## Direct Fuel

Biosolids from sewage have been heavily researched and developed for use as fuels due to their ever-increasing volume and broad availability. Although little work has been done on



Photo from iStock 468667512

food waste digestate in this area, there is little reason to think it would not be just as suitable. One recent study looked at co-combusting with municipal solid waste, and although the food waste digestate had a lower energy content, blending with municipal solid waste mitigated this to some extent and was still feasible.<sup>33</sup> Biosolids, and potentially food waste digestate, can be used as fuel in multiple ways. After drying, the biosolids can be burned directly, usually in a fluidized bed incinerator, generating both heat and potentially power. In Europe, electricity generation from this can command higher prices due to the “green” status of the production. The additional advantage is that the solids volume is greatly reduced, with stabilized inorganic ash being primarily the only residue created. The downside is that emissions require mitigation, and some of the energy recovered is required to dry the material before burning it. Similar to incineration, co-firing of biosolids in existing coal- or biomass-fed power plants provides power from the digestate and takes advantage of existing combustion, generation, and emission control infrastructure.<sup>34</sup> A potentially major outlet for biosolids is co-firing in cement kilns. This is currently used in Europe and presents the advantages of (1) disposing biosolids, (2) displacing fossil fuels used in cement manufacturing, and (3) incorporating the resultant ash into cement.<sup>35</sup>

Fuel pellets made from drying and forming biosolids and co-fired with coal or wood pellets have been researched and proposed for years, but commercial adoption has lagged.<sup>36-38</sup> Multiple studies have reported that co-firing with more traditional fuels demonstrates no issues, but commercial implementation has not been carried out on any great scale.<sup>39</sup> A major obstacle is the high cost of solid-liquid separation needed to produce dry pellets. Small AD operations are limited

in their ability to economically produce these pellets due to their low production volume; however, large municipal facilities or combined small-scale operations are likely to reduce this cost considerably into the economical range.<sup>38</sup> An advantage of this process is that phosphorus can be sequestered into the pellets instead of being discharged with the spent centrate. Not only does this remove and concentrate the phosphorus, but it has also been shown to eliminate pathogens such as *Clostridium* spp.<sup>40</sup> When burned, the resultant high-phosphorous ash can be used in fertilizer production.<sup>38</sup> Though not specifically related to fuel applications, digestate pellets could also be used as soil amendment; however, it has been shown that digestate pellets produce significant N<sub>2</sub>O emissions when applied on soils.<sup>41</sup> Recently, several companies have begun to market digestate pelleting operations and equipment for both fuel and fertilizer pellets (e.g., Elf Systems, Nawrocki Pelleting Technology, and Kesir).<sup>42-44</sup>

### Indirect Fuel and Products

High-strength centrate has been used to stimulate algae growth in treatment ponds, where the algae clean the water by removing nutrients (mainly nitrogen and phosphorous) and the algae are subsequently processed to produce biofuels or bioproducts.<sup>45-47</sup> Recent interest in diverting carbon away from biogas and toward liquid fuels and products is leaning towards production of VFAs and/or longer-chain alcohols by arresting methanogenesis. In this process, the methanogens are inhibited chemically, thermally, or physiologically (low/high pH), and VFAs are allowed to build up in the centrate. Separating the VFAs from the centrate using mechanical, physical, electrochemical, or other means mimics the methanogenesis and allows the hydrolysis, acidogenesis, and acetogenesis to continue while

providing a higher-value stream of VFAs to serve as feedstock chemicals for catalytic or biological upgrading to hydrocarbon fuels, higher alcohols, or other bioproducts. This work is still preliminary, but it holds much promise for valorizing AD operations beyond just methane.

## Water

The centrate, or liquid fraction, of the digestate contains both soluble compounds and water. Aerobic water treatment is often used to biologically “combust” the soluble organics in low-strength wastewater to CO<sub>2</sub>. Combined with settling/filtration and other treatment steps, both potable and irrigation water can be produced. Likewise, the centrate can also be recycled back into the AD process to provide process water if needed.

## Bio-Oil, Biochar, and Syngas

Biosolids can be transformed into liquid and gaseous fuels using thermal or thermocatalytic processing. Pyrolysis, gasification, and hydrothermal liquefaction are all proposed routes to convert biosolids to such products, but pyrolysis is a bit behind in the technology development. The technology readiness levels for pyrolysis, gasification, and hydrothermal liquefaction are 5, 6–7, and 6, respectively. The primary differences between these technologies are in the parameters used (moisture, temperature, and pressure), which determine the products formed, the fraction of each, and extent of conversion.

Gasification (>800°C, some O<sub>2</sub> present) generally produces syngas (CO and H<sub>2</sub>), as well as tar—a major problematic byproduct. The biosolids must also be dried first. At least one gasification demonstration facility has been in operation in Tokyo since 2010.<sup>48</sup> Pyrolysis (400°C–600°C, no O<sub>2</sub>) produces mainly H<sub>2</sub>, CO, CO<sub>2</sub>, CH<sub>4</sub>, bio-oil, and char. Pyrolysis requires low moisture, mid-temperatures, and lower pressures compared to hydrothermal liquefaction, which has lower temperatures but higher pressure and can handle large amounts of water.

Thermo-catalytic reforming<sup>49</sup> and hydrothermal processing are thermal processes that convert organic waste into several fuel-type product streams—primarily bio-oil (bio-crude), syngas, and H<sub>2</sub>. Biochar or hydrochar is also produced and can be used as a soil conditioner/fertilizer and carbon sequestration mechanism.<sup>50, 51</sup> Biochar has been shown to increase methane production in high-solid digesters by fostering microbial interaction and increasing the fractional methane content by adsorbing CO<sub>2</sub>.<sup>17, 52</sup> As a soil conditioner, biochar can provide slow release of phosphorus and help sequester nitrogen.<sup>53, 54</sup> Lastly, multiple studies have examined the use of biochar to adsorb metals, nutrients, and contaminants from digestate.<sup>55–60</sup> The thermo-catalytic reforming process being developed by the European Union in its TO-SYN-FUEL project uses dried biosolids as a feedstock, but food waste digestate should be amenable as well. The primary products of thermo-catalytic reforming are syngas, bio-oil, and H<sub>2</sub>.<sup>49</sup> Over a pyrolysis temperature range, food waste pyrolysis has been shown to produce the typical

yields of bio-oil (17% at 400°C to 23% at 700°C), biochar (64% at 400°C down to 52% at 700°C), and syngas (18% at 400°C to 25% at 700°C).<sup>61</sup>

Hydrothermal processing handles wet organic material, as water is part of the reaction, and can be divided into hydrothermal liquefaction (200°C–400°C) and hydrothermal carbonization (180°C–250°C). Hydrothermal liquefaction produces bio-oil, syngas, and biochar, whereas hydrothermal carbonization produces mostly CO<sub>2</sub> and hydrochar.<sup>62</sup> For any of these processes, the syngas can be burned directly or used to make fuels like diesel. Bio-oil can also be burned in heavy engines or refined into diesel, jet, and gasoline-like fuels. Bio-oil generally requires cleanup and processing before use and is not optimal for standard internal combustion engines, though this can be addressed by different engine designs. Water recovered from either process can be reprocessed at the water resource recovery facility or fed back into the digester. Currently, this technology is being applied to biosolids, though food waste digestate would serve as well.

One other interesting approach is to combine produced syngas with the AD step. The CO<sub>2</sub> and H<sub>2</sub> in the syngas can be reformed into CH<sub>4</sub> in the digester, increasing CH<sub>4</sub> yields and titers.<sup>61</sup>

## Other Uses

After dewatering and drying, digestate is often used for animal bedding.<sup>63</sup> Although this is a low-cost and mostly local outlet, the bedding often ends up back in a digester, thus increasing the ultimate extent of conversion of the original food waste. Other examples include using food waste digestate to grow edible mushrooms, as published by one clever graduate student,<sup>63</sup> or as a nutrient source to grow



Photo from iStock 808876934

algae for biofuel production,<sup>64</sup> similar to other liquid digestates. Research at Michigan State University indicates that medium-density fiberboard and fiber-plastic composites can also be manufactured successfully from digestate solids.<sup>65</sup>

## Takeaways

The main utilization options for food waste digestate currently revolve around land application or animal bedding. There are some demonstration technologies in place or being built to evaluate thermal conversion of biosolids to fuels and biochar, and several companies are promoting these options, but they are not yet fully commercialized, and research needs to be done to validate that food waste will perform similarly to biosolids. Several companies have proposed pelletizing biosolids for use as a co-fuel with wood pellets, and although food waste digestate could be just as effective, there are no commercial or even pilot operations at the moment. Part of the lack of information and demonstration is the relatively low level of food waste digestion operations compared to sewage and manure. As food waste becomes a larger fraction of AD feedstocks in both stand-alone and co-digestion facilities, operators will need to test these various technologies to empirically determine their utility and economics.

## Suggested Citation

Decker, Stephen R., and Anelia Milbrandt. 2022. *Anaerobic Digestion of Food Waste: Products and Their Uses*. Golden, CO: National Renewable Energy Laboratory. NREL/BR-2700-81676. <https://www.nrel.gov/docs/fy22osti/81676.pdf>.

## References

1. Boontian, N., Conditions of the Anaerobic Digestion of Biomass. *International Journal of Environmental and Ecological Engineering* **2014**, 8 (9), 5.
2. Álvarez, J. A.; Otero, L.; Lema, J. M., A methodology for optimising feed composition for anaerobic co-digestion of agro-industrial wastes. *Bioresource Technology* **2010**, 101 (4), 1153-1158.
3. Cavinato, C.; Bolzonella, D.; Pavan, P.; Fatone, F.; Cecchi, F., Mesophilic and thermophilic anaerobic co-digestion of waste activated sludge and source sorted biowaste in pilot- and full-scale reactors. *Renewable Energy* **2013**, 55, 260-265.
4. Cavinato, C.; Fatone, F.; Bolzonella, D.; Pavan, P., Thermophilic anaerobic co-digestion of cattle manure with agro-wastes and energy crops: Comparison of pilot and full scale experiences. *Bioresource Technology* **2010**, 101 (2), 545-550.
5. Wang, Y.; Li, G.; Chi, M.; Sun, Y.; Zhang, J.; Jiang, S.; Cui, Z., Effects of co-digestion of cucumber residues to corn stover and pig manure ratio on methane production in solid state anaerobic digestion. *Bioresource Technology* **2018**, 250, 328-336.
6. Valenti, F.; Zhong, Y.; Sun, M.; Porto, S. M. C.; Toscano, A.; Dale, B. E.; Sibilla, F.; Liao, W., Anaerobic co-digestion of multiple agricultural residues to enhance biogas production in southern Italy. *Waste Management* **2018**, 78, 151-157.
7. Siddique, M. N. I.; Wahid, Z. A., Achievements and perspectives of anaerobic co-digestion: A review. *Journal of Cleaner Production* **2018**, 194, 359-371.
8. Arreola-Vargas, J.; Ojeda-Castillo, V.; Snell-Castro, R.; Corona-González, R. I.; Alatríste-Mondragón, F.; Méndez-Acosta, H. O., Methane production from acid hydrolysates of Agave tequilana bagasse: Evaluation of hydrolysis conditions and methane yield. *Bioresource Technology* **2015**, 181, 191-199.
9. Aslanzadeh, S., Pretreatment of cellulosic waste and high rate biogas production. 2014; p 168.
10. Barrios, J. A.; Duran, U.; Cano, A.; Cisneros-Ortiz, M.; Hernandez, S., Sludge electrooxidation as pre-treatment for anaerobic digestion. *Water Sci Technol* **2017**, 75 (3-4), 775-781.
11. Braguglia, C. M.; Gianico, A.; Gallipoli, A.; Mininni, G., The impact of sludge pre-treatments on mesophilic and thermophilic anaerobic digestion efficiency: Role of the organic load. *Chemical Engineering Journal* **2015**, 270, 362-371.
12. Carrere, H.; Sialve, B.; Bernet, N., Improving pig manure conversion into biogas by thermal and thermo-chemical pretreatments. *Bioresource Technology* **2009**, 100 (15), 3690-4.
13. Čater, M.; Zorec, M.; Marinšek Logar, R., Methods for Improving Anaerobic Lignocellulosic Substrates Degradation for Enhanced Biogas Production. *Springer Science Reviews* **2014**, 2 (1-2), 51-61.
14. Ruan, D.; Zhou, Z.; Pang, H.; Yao, J.; Chen, G.; Qiu, Z., Enhancing methane production of anaerobic sludge digestion by microaeration: Enzyme activity stimulation, semi-continuous reactor validation and microbial community analysis. *Bioresource Technology* **2019**, 289, 121643.
15. Are Ancient Bugs the Key to Storing Wind and Solar? <https://www.greentechmedia.com/articles/read/are-ancient-bugs-the-key-to-storing-wind-and-solar>.
16. Prajapati, S. K.; Kumar, P.; Malik, A.; Vijay, V. K., Bioconversion of algae to methane and subsequent utilization of digestate for algae cultivation: a closed loop bioenergy generation process. *Bioresource Technology* **2014**, 158, 174-80.
17. Wang, Z.; Wang, S.; Xie, S.; Jiang, Y.; Meng, J.; Wu, G.; Hu, Y.; Zhan, X., Stimulatory effects of biochar addition on dry anaerobic co-digestion of pig manure and food waste under mesophilic conditions. *Environ Sci Pollut Res Int* **2021**.

18. Erkan, M.; Sanin, F. D., Can sludge dewatering reactivate microorganisms in mesophilically digested anaerobic sludge? Case of belt filter versus centrifuge. *Water Res* **2013**, *47* (1), 428-38.
19. Cao, B.; Zhang, T.; Zhang, W.; Wang, D., Enhanced technology based for sewage sludge deep dewatering: A critical review. *Water Res* **2021**, *189*, 116650.
20. Ginisty, P.; Mailler, R.; Rocher, V., Sludge conditioning, thickening and dewatering optimization in a screw centrifuge decanter: Which means for which result? *J Environ Manage* **2021**, *280*, 111745.
21. He, X.; He, L.; Lin, Z.; Zhou, J.; Shi, S.; Liu, Y.; Zhou, J., Deep dewatering of activated sludge using composite conditioners of surfactant, acid and flocculant: The mechanism and dosage model. *Sci Total Environ* **2021**, 150899.
22. Hu, P.; Shen, S.; Zhao, D.; Wei, H.; Ge, J.; Jia, F.; Zhang, X.; Yang, H., The influence of hydrophobicity on sludge dewatering associated with cationic starch-based flocculants. *J Environ Manage* **2021**, *296*, 113218.
23. Hui, K.; Song, L.; Yin, Z.; Song, H.; Wang, Z.; Gao, W.; Xuan, L., Freeze-thaw combined with activated carbon improves electrochemical dewaterability of sludge: analysis of sludge floc structure and dewatering mechanism. *Environ Sci Pollut Res Int* **2021**.
24. Kim, H. J.; Chon, K.; Lee, Y. G.; Kim, Y. K.; Jang, A., Enhanced mechanical deep dewatering of dewatered sludge by a thermal hydrolysis pre-treatment: Effects of temperature and retention time. *Environ Res* **2020**, *188*, 109746.
25. Li, E.; Wang, Y.; Zhang, D.; Fan, X.; Han, Z.; Yu, F., Siderite/PMS conditioning-pressurized vertical electro-osmotic dewatering process for activated sludge volume reduction: Evolution of protein secondary structure and typical amino acid in EPS. *Water Res* **2021**, *201*, 117352.
26. Lv, H.; Xiong, Q.; Liu, D.; Wu, X., Coupling electro-dewatering and low-temperature air-drying for efficient dewatering of sludge. *Sci Rep* **2021**, *11* (1), 19167.
27. Rao, B.; Su, X.; Lu, X.; Wan, Y.; Huang, G.; Zhang, Y.; Xu, P.; Qiu, S.; Zhang, J., Ultrahigh pressure filtration dewatering of municipal sludge based on microwave pretreatment. *J Environ Manage* **2019**, *247*, 588-595.
28. Wakeman, R. J., Separation technologies for sludge dewatering. *J Hazard Mater* **2007**, *144* (3), 614-9.
29. Wei, H.; Gao, B.; Ren, J.; Li, A.; Yang, H., Coagulation/flocculation in dewatering of sludge: A review. *Water Res* **2018**, *143*, 608-631.
30. Wu, B.; Dai, X.; Chai, X., Critical review on dewatering of sewage sludge: Influential mechanism, conditioning technologies and implications to sludge re-utilizations. *Water Res* **2020**, *180*, 115912.
31. Bloom, About Bloom. <https://bloomsoil.com/about-bloom-soil-amendment>.
32. Tampio, E.; Marttinen, S.; Rintala, J., Liquid fertilizer products from anaerobic digestion of food waste: mass, nutrient and energy balance of four digestate liquid treatment systems. *Journal of Cleaner Production* **2016**, *125*, 22-32.
33. Wei, C.; Yu, Z.; Zhang, X.; Ma, X., Co-combustion behavior of municipal solid waste and food waste anaerobic digestates: Combustion performance, kinetics, optimization, and gaseous products. *Journal of Environmental Chemical Engineering* **2021**, *9* (5).
34. Roy, M. M.; Dutta, A.; Corscadden, K.; Havard, P.; Dickie, L., Review of biosolids management options and co-incineration of a biosolid-derived fuel. *Waste Manag* **2011**, *31* (11), 2228-35.
35. Lechtenberg, D. Use of Sewage Sludge in Cement Industry. <https://www.bioenergyconsult.com/sewage-cement-industry/>.
36. Roy, M. M.; Dutta, A.; Corscadden, K.; Havard, P., Co-combustion of Biosolids with Wood Pellets in a Wood Pellet Stove. *International Journal of Engineering & Technology* **2011**, *11* (3), 7-15.
37. Nagy, D.; Balogh, P.; Gabnai, Z.; Popp, J.; Oláh, J.; Bai, A., Economic Analysis of Pellet Production in Co-Digestion Biogas Plants. *Energies* **2018**, *11* (5).
38. Cathcart, A.; Smyth, B. M.; Lyons, G.; Murray, S. T.; Rooney, D.; Johnston, C. R., An economic analysis of anaerobic digestate fuel pellet production: can digestate fuel pellets add value to existing operations? *Cleaner Engineering and Technology* **2021**, *3*.
39. Pedrazzi, S.; Allesina, G.; Belló, T.; Rinaldini, C. A.; Tartarini, P., Digestate as bio-fuel in domestic furnaces. *Fuel Processing Technology* **2015**, *130*, 172-178.
40. Pulvirenti, A.; Ronga, D.; Zaghi, M.; Tomasselli, A. R.; Mannella, L.; Pecchioni, N., Pelleting is a successful method to eliminate the presence of Clostridium spp. from the digestate of biogas plants. *Biomass and Bioenergy* **2015**, *81*, 479-482.
41. Petrova, I. P.; Ruser, R.; Guzman-Bustamante, I., Pellets from Biogas Digestates: A Substantial Source of N<sub>2</sub>O Emissions. *Waste and Biomass Valorization* **2020**, *12* (5), 2433-2444.
42. Elf Systems, Pellet Mills for Sale. **2021**. <https://elfpelletmills.com/>.
43. Nawrocki Pelleting Technology. **2021**. <https://www.nawrockipt.co.uk/>.
44. Kesir, Make Fertiliser & Digestate Pellets. **2021**. <https://makepellets.co.uk/fertilizer-and-digestate-pellets/>.

45. Krustok, I.; Diaz, J. G.; Odlare, M.; Nehrenheim, E., Algae biomass cultivation in nitrogen rich biogas digestate. *Water Sci Technol* **2015**, 72 (10), 1723-9.
46. Pizzera, A.; Scaglione, D.; Bellucci, M.; Marazzi, F.; Mezzanotte, V.; Parati, K.; Ficara, E., Digestate treatment with algae-bacteria consortia: A field pilot-scale experimentation in a sub-optimal climate area. *Bioresource Technology* **2019**, 274, 232-243.
47. Xu, J.; Zhao, Y.; Zhao, G.; Zhang, H., Nutrient removal and biogas upgrading by integrating freshwater algae cultivation with piggy anaerobic digestate liquid treatment. *Appl Microbiol Biotechnol* **2015**, 99 (15), 6493-501.
48. Metawater Wastewater sludge gasification power generation system. [https://www.metawater.co.jp/eng/solution/product/sewer/gas\\_convert/](https://www.metawater.co.jp/eng/solution/product/sewer/gas_convert/).
49. 2synfuel, Thermo-Catalytic Reforming (TCR®) in demonstration scale to convert biogenic residues into different products for a low carbon economy. **2020**.
50. Tayibi, S.; Monlau, F.; Marias, F.; Thevenin, N.; Jimenez, R.; Oukarroum, A.; Alboukhas, A.; Zeroual, Y.; Barakat, A., Industrial symbiosis of anaerobic digestion and pyrolysis: Performances and agricultural interest of coupling biochar and liquid digestate. *Sci Total Environ* **2021**, 793, 148461.
51. Breunig, H. M.; Amirebrahimi, J.; Smith, S.; Scown, C. D., Role of Digestate and Biochar in Carbon-Negative Bioenergy. *Environ Sci Technol* **2019**, 53 (22), 12989-12998.
52. Lee, J. T. E.; Ok, Y. S.; Song, S.; Dissanayake, P. D.; Tian, H.; Tio, Z. K.; Cui, R.; Lim, E. Y.; Jong, M. C.; Hoy, S. H.; Lum, T. Q. H.; Tsui, T. H.; Yoon, C. S.; Dai, Y.; Wang, C. H.; Tan, H. T. W.; Tong, Y. W., Biochar utilisation in the anaerobic digestion of food waste for the creation of a circular economy via biogas upgrading and digestate treatment. *Bioresource Technology* **2021**, 333, 125190.
53. Shanmugam, S.; Jenkins, S. N.; Mickan, B. S.; Jaafar, N. M.; Mathes, F.; Solaiman, Z. M.; Abbott, L. K., Co-application of a biosolids product and biochar to two coarse-textured pasture soils influenced microbial N cycling genes and potential for N leaching. *Sci Rep* **2021**, 11 (1), 955.
54. Figueiredo, C. C.; Pinheiro, T. D.; de Oliveira, L. E. Z.; de Araujo, A. S.; Coser, T. R.; Paz-Ferreiro, J., Direct and residual effect of biochar derived from biosolids on soil phosphorus pools: A four-year field assessment. *Sci Total Environ* **2020**, 739, 140013.
55. Wang, Y.; Song, Y.; Li, N.; Liu, W.; Yan, B.; Yu, Y.; Liang, L.; Chen, G.; Hou, L.; Wang, S., Tunable active sites on biogas digestate derived biochar for sulfanilamide degradation by peroxymonosulfate activation. *J Hazard Mater* **2022**, 421, 126794.
56. Wang, H.; Xiao, K.; Yang, J.; Yu, Z.; Yu, W.; Xu, Q.; Wu, Q.; Liang, S.; Hu, J.; Hou, H.; Liu, B., Phosphorus recovery from the liquid phase of anaerobic digestate using biochar derived from iron-rich sludge: A potential phosphorus fertilizer. *Water Res* **2020**, 174, 115629.
57. Huang, S.; Wang, T.; Chen, K.; Mei, M.; Liu, J.; Li, J., Engineered biochar derived from food waste digestate for activation of peroxymonosulfate to remove organic pollutants. *Waste Manag* **2020**, 107, 211-218.
58. Jiang, B.; Lin, Y.; Mbog, J. C., Biochar derived from swine manure digestate and applied on the removals of heavy metals and antibiotics. *Bioresource Technology* **2018**, 270, 603-611.
59. Kocaturk-Schumacher, N. P.; Zwart, K.; Bruun, S.; Brussaard, L.; Jensen, L. S., Does the combination of biochar and clinoptilolite enhance nutrient recovery from the liquid fraction of biogas digestate? *Environ Technol* **2017**, 38 (10), 1313-1323.
60. Fu, D.; Chen, Z.; Xia, D.; Shen, L.; Wang, Y.; Li, Q., A novel solid digestate-derived biochar-Cu NP composite activating H<sub>2</sub>O<sub>2</sub> system for simultaneous adsorption and degradation of tetracycline. *Environmental Pollution (Barking, Essex : 1987)* **2017**, 221, 301-310.
61. Yang, Z.; Liu, Y.; Zhang, J.; Mao, K.; Kurbonova, M.; Liu, G.; Zhang, R.; Wang, W., Improvement of biofuel recovery from food waste by integration of anaerobic digestion, digestate pyrolysis and syngas biomethanation under mesophilic and thermophilic conditions. *Journal of Cleaner Production* **2020**, 256.
62. Chen, W. T.; Haque, M. A.; Lu, T.; Aierzhati, A.; Reimonn, G., A perspective on hydrothermal processing of sewage sludge. *Curr Opin Environ Sci Health* **2020**, 14, 63-73.
63. O'Brien, B. J.; Milligan, E.; Carver, J.; Roy, E. D., Integrating anaerobic co-digestion of dairy manure and food waste with cultivation of edible mushrooms for nutrient recovery. *Bioresource Technology* **2019**, 285, 121312.
64. Chuka-ogwude, D.; Ogbonna, J.; Moheimani, N. R., A review on microalgal culture to treat anaerobic digestate food waste effluent. *Algal Research* **2020**, 47.
65. Renewable Carbon News, Fiber from anaerobic digesters used to develop wood-plastic composites. **2008**. <https://renewable-carbon.eu/news/fiber-from-anaerobic-digesters-used-to-develop-wood-plastic-composites/>.